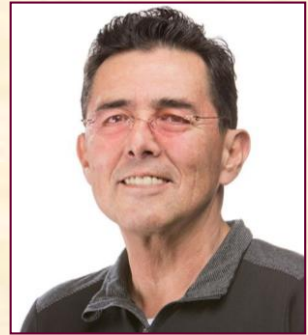


ON PUMP SEALS OPERATING WITH MULTIPLE PHASE CONDITIONS: MEASUREMENTS AND GAS INJECTION TO INCREASE SEAL CENTERING STIFFNESS

Luis San Andres



A dinosaur!



Luis San Andres

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Turbomachinery Lab →
Texas A&M University



Luis performs research in lubrication and rotordynamics. He is a Fellow of ASME, STLE, GPPS, and a member of the Industrial Advisory Committees for the TEES Turbomachinery Symposia (Houston & Asia). Luis has published over 200 peer reviewed papers, several recognized as best in various conferences.

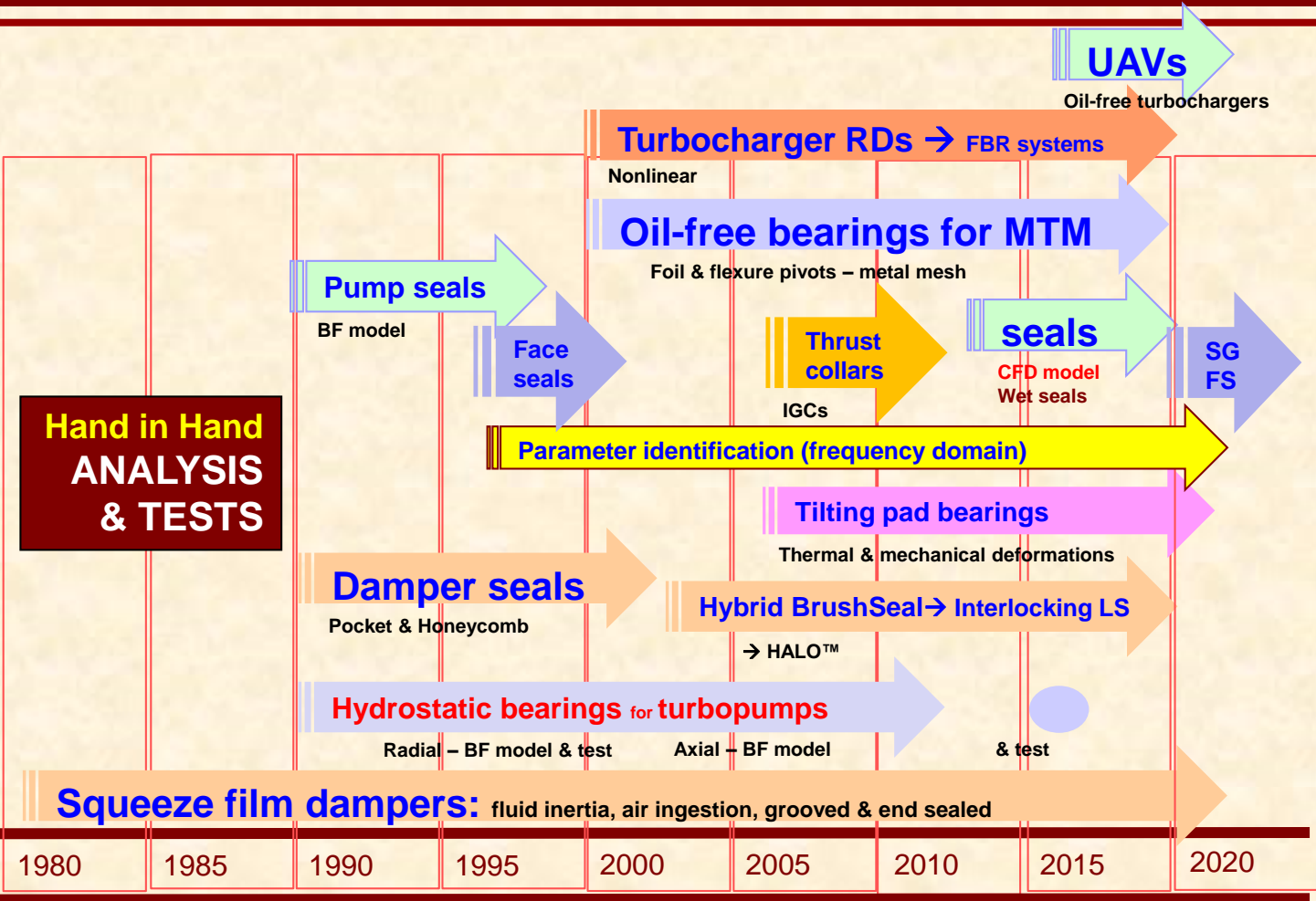
In 2022, ASME-IGTI bestowed Luis with the Aircraft Engine Technology Award (AETA) for sustained creative contributions to the field.



A dinosaur walk since last millennium

Funding Sources

John Crane, Baker-Hughes, Trane, Elliott Co.
 Blue Origin,
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 Danfoss TurboCor
 Borg-Warner TC,
 Torishima Pumps
 MHI, Hitachi RL,
 Samsung, Key Yang,
 Hyundai HI, Capstone MT
 Siemens TRC



Co-chaired 1st WTC, London 1997



A need: subsea pumping & compression

Subsea Engineering or SURF

Subsea

Umbilicals

Risers

Flowlines

Wet compression
systems a must!

High pressure & extreme temperature

A 3D rendering of subsea oil production facilities on the ocean floor. The scene shows several yellow and black structures (platforms) connected by a network of yellow flowlines. The background is a deep blue ocean with a sandy seabed.

Bloomberg 7/30/19: Offshore oil production tops shale oil on generation of jobs.

Extreme engineering enables five year or longer reliability for subsea production facilities (North Sea & Brazil → Gulf of Mexico → Arctic).

The need

Wet gas compression and multiphase oil boosting save up to 30% in CAPEX compared with a L/G separation station.

Wet compressors must operate with up to 5% in liquid volume fraction (LVF) and multiple phase pumps with up to 90% in gas volume fraction (GVF)



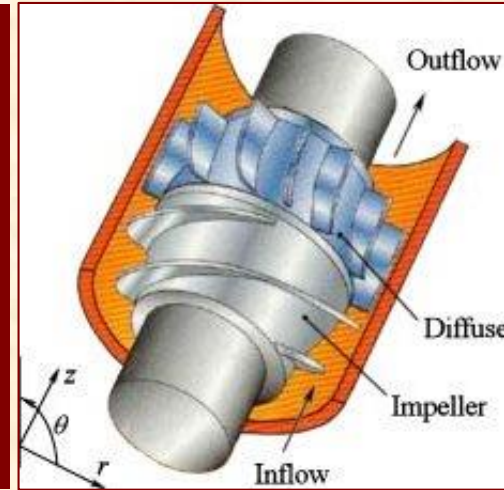
Known that seals operating under a *wet gas or bubbly flow condition* affect system rotordynamic stability



Need of concerted effort to quantify effect of two phase flow in sealing components →

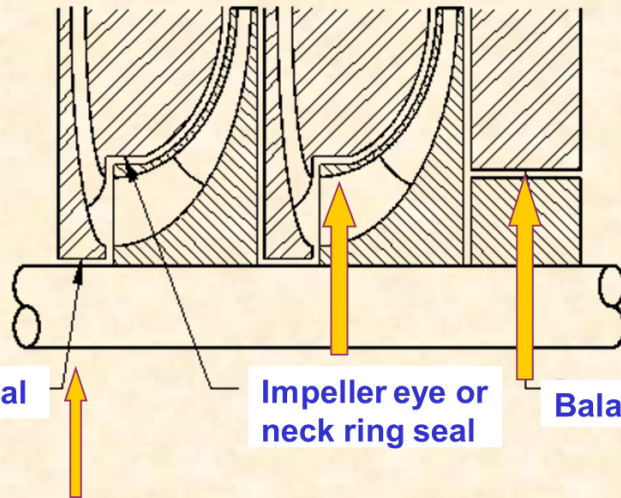
towards improving reliability and reducing operational costs.

Current knowledge



Cost efficient subsea factories must rely on multiple-phase flow compression and pump systems that reduce tieback systems and perform full flow separation on the sea floor, but.....

Annular Pressure Seals



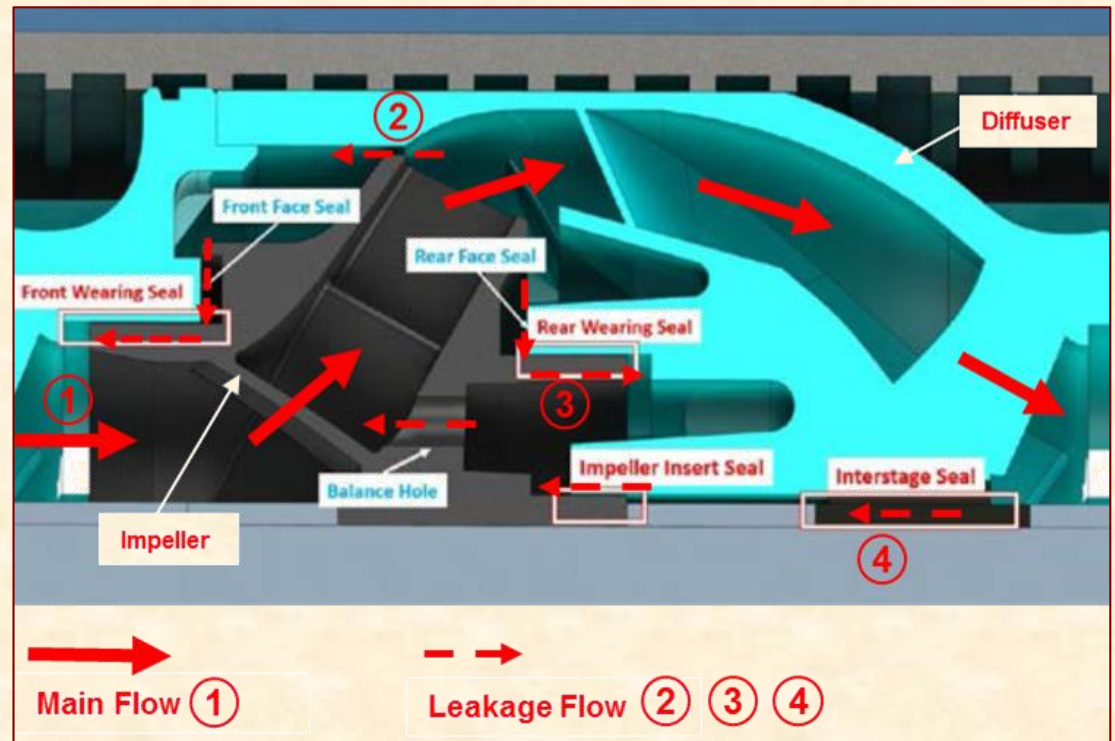
Inter-stage seal

Impeller eye or neck ring seal

Balance piston seal

separate regions of high pressure and low pressure to **minimize the leakage** (secondary flow).

Multiple phase pump



Main Flow (1)

Leakage Flow (2) (3) (4)

Two-phase flow in a wet gas compressor

Rotor lateral vibration

13.5 krpm, 10 bar

Balance piston:
Labyrinth seal

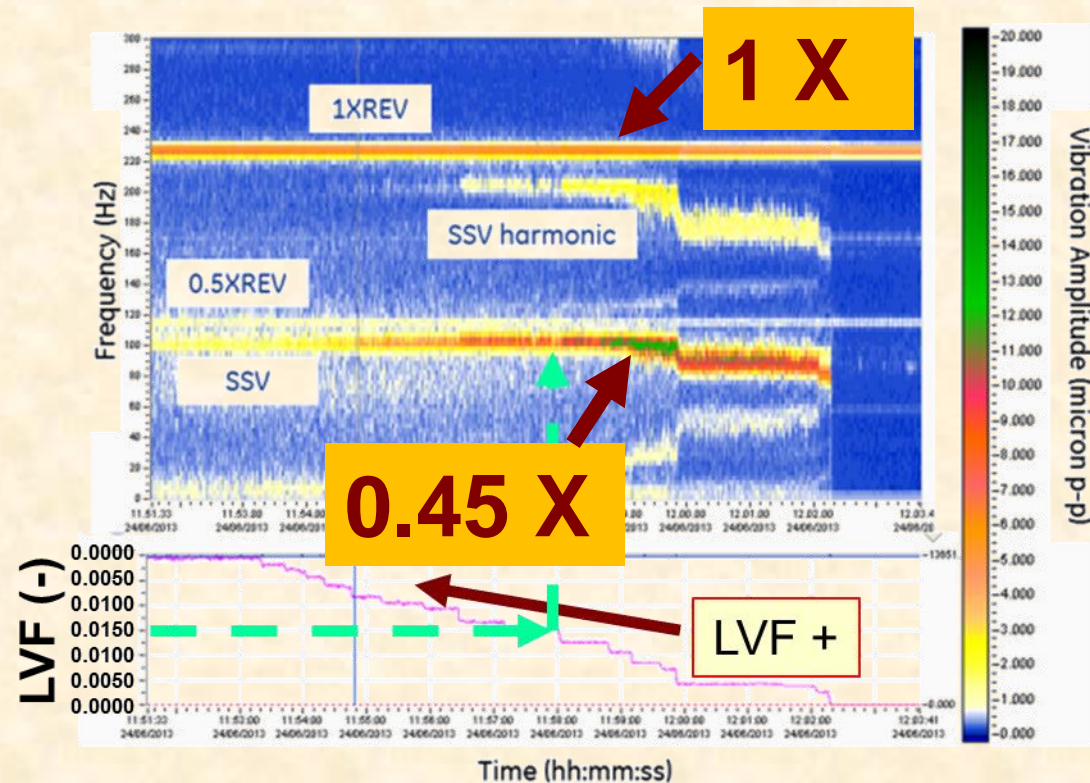


Fluids:
Air and water

LVF: 0~3%

0.45 X SSV increases in
magnitude with LVF

Trapped liquid in seal
rotates and causes SSV



Vannini et al., 2016, "Experimental Results and CFD Simulations of Labyrinth and Pocket Damper Seals for Wet Gas Compression," ASME J. Eng. Gas Turb. Power, **138**, p. 052501.

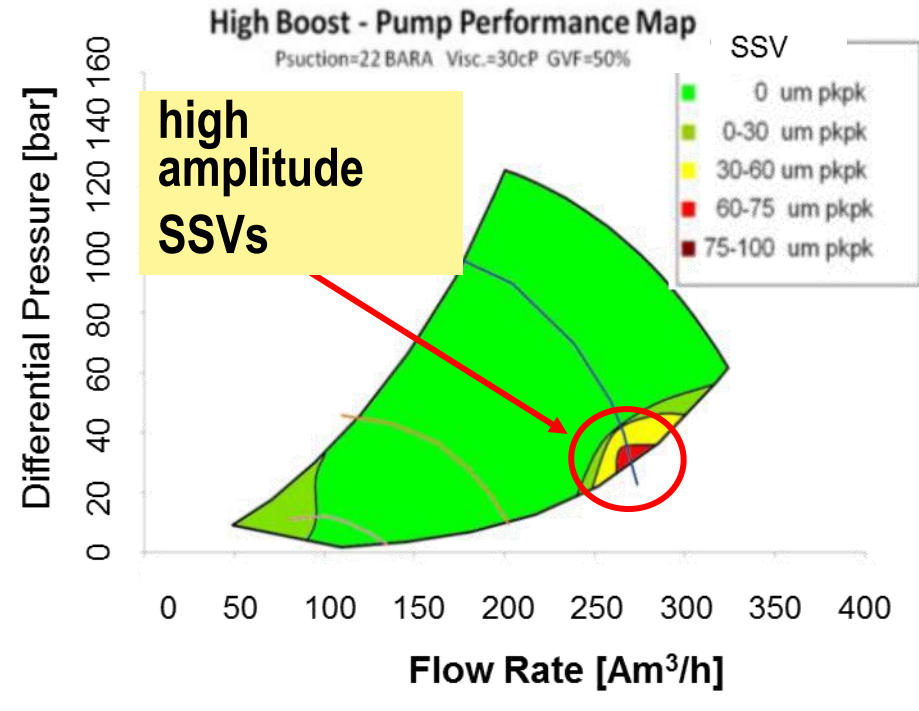
Two-phase flow in a pump

Helico-axial pump (1.5 to 4.6 krpm)

Pump operates stable with liquid.
(600 cPoise)

Rotor SSV appears under some two-phase flow conditions : **low differential pressure with a high-viscosity mixture.**

When SSV occurs, rotor **whirl frequency ratio > 1.0.**



Bibet et al. (2013)

Bibet, P. J., et al., 2013, "Design and Verification Testing of a New Balance Piston for High Boost Multiphase Pumps," Proc. 29th International Pump User Symposium, Houston, TX.

In the subsea oil and gas industry, multiphase pumps and wet gas compressors enable long distance tie back system and eliminate oil and gas separation stations.

Seals must be able to operate without affecting the system efficiency and dynamic stability.

The lecture presents measurements of leakage and force coefficients for five clearance seals operating with an air in oil mixture ranging from pure liquid to mostly air.

Queries of interest

1. Why *wet* (bubbly) seals? Where are they found?
2. How does gas content affect seal leakage and drag?
3. How does gas content affect the stiffness and damping coefficients of a *wet* seal?
4. Why a wavy surface seal is a better option than a plain seal for a two phase flow pump?
5. Why gas injection increases the centering stiffness of seals in pumps & hydraulic turbines?

Pros/cons of **two-phase flow** operation

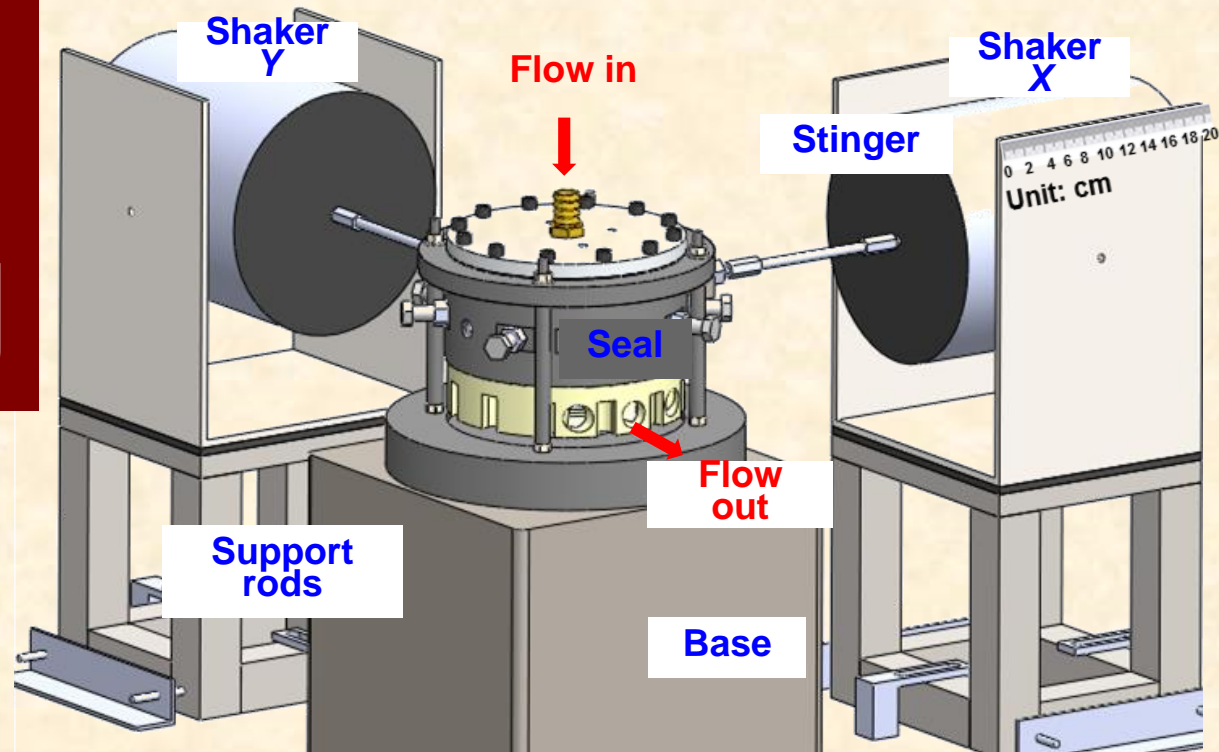
	Multiphase pumping	Wet gas compression	Hydraulic turbine/pumps
Applications	Onshore, offshore, subsea and downhole GVF 0 -100% [1]	Subsea and downhole LVF 0 – 5% [2]	Power generation
Benefits	Add pressure to process fluids, enabling long distance tie back system to reduce O&G separation stations. Cost drops ~ 30%		Clean energy
Challenges	Rotor sub-synchronous vibrations		Often suffer from non-synchronous vibration even at null speed [3]

[1] **Gong, H., et al., 2012**, "Comparison of Multiphase Pumping Technologies for Subsea and Downhole Applications." *Oil and Gas Facilities*, 1(01), pp. 36-46.

[2] **Vannini, G., et al., 2014**, "Centrifugal Compressor Rotordynamics in Wet Gas Conditions." *Proc. of the 43th Turbomachinery & 30th Pump Users Symposia*, Houston, TX, September 23-25.

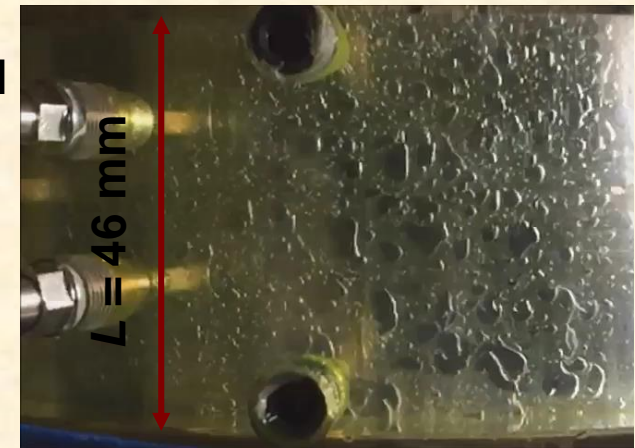
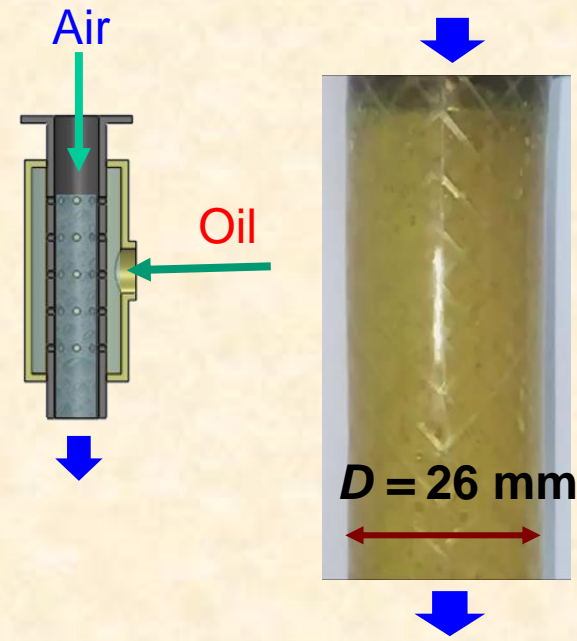
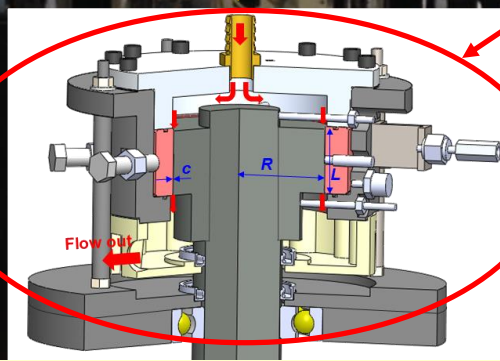
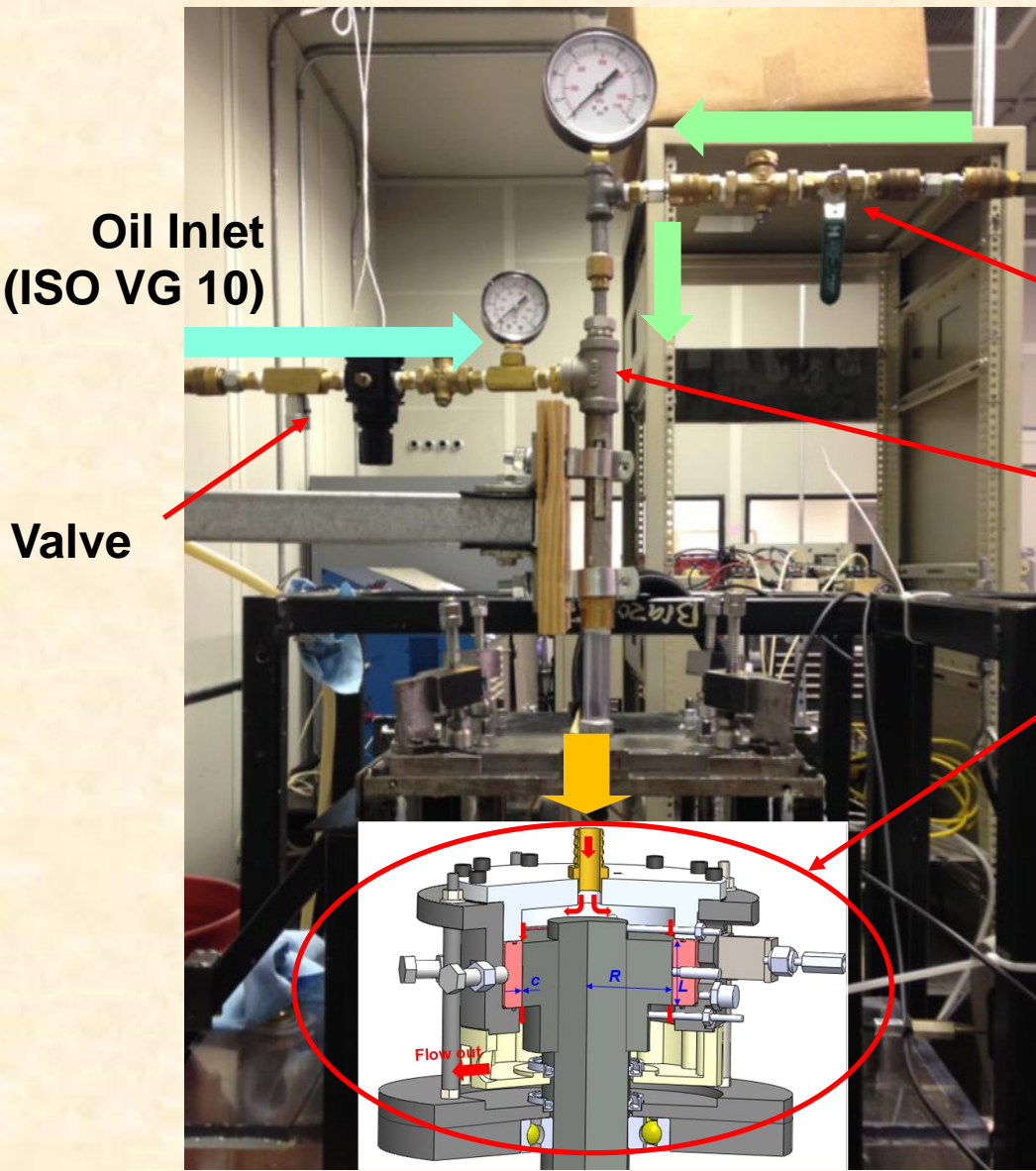
[3] **Smith, et al., 1996**, "Centrifugal Pump Vibration Caused by Supersynchronous Shaft Instability Use of Pumpout Vanes to Increase Pump Shaft Stability." *Proc. 13th International Pump Users Symposium*, Houston, TX, Mar. 5-7.

Wet Gas Test Rig



- **Controlled motion test rig with "floating" seal housing and centered with spinning rigid shaft.**
- **Shakers exert frequency-dependent loads to excite system toward obtaining seal force coefficients.**

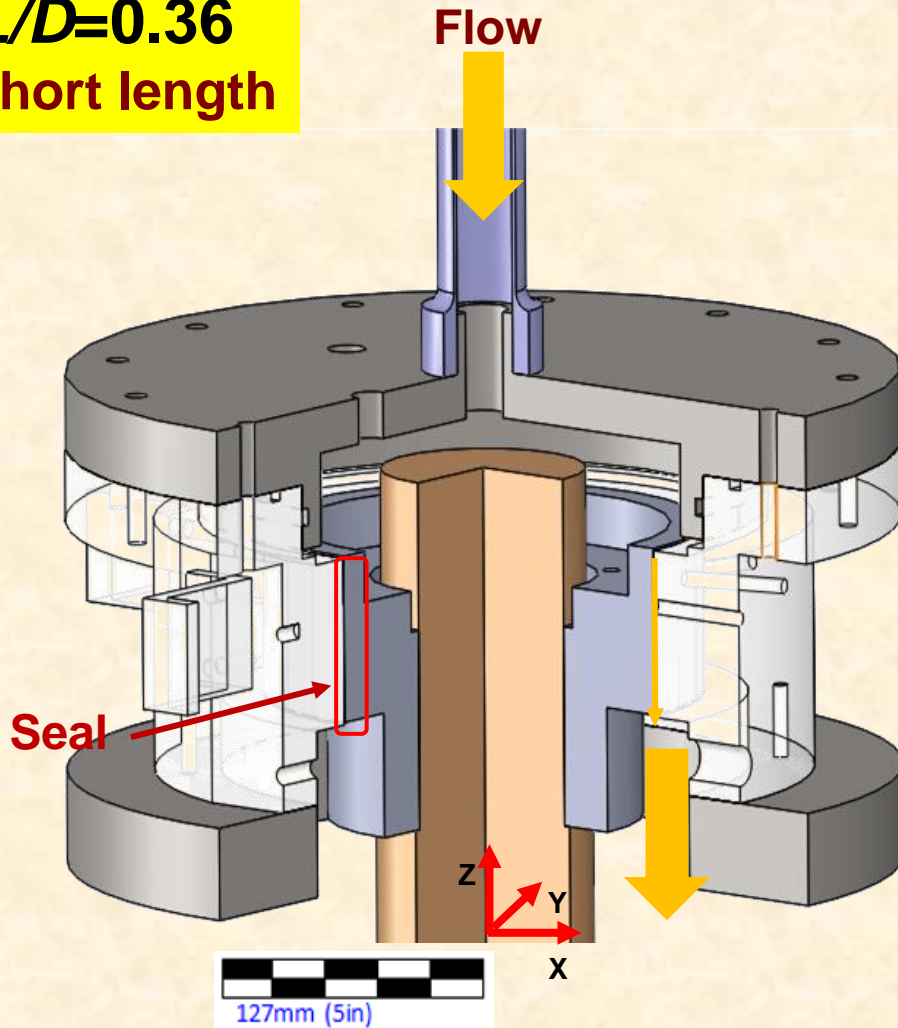
Wet seal test rig



journal speed: 3.5 krpm (23.3 m/s)

$P_s/P_a=2.5$, inlet GVF=50%, stationary shaft

$L/D=0.36$
short length



Seals	
Diameter (D)	127 mm (5 in)
Length (L)	46 mm (1.8 in)
Clearance (c) 34 °C	0.203 mm (8 mil)
Supply pressure (P_s)	1.0~3.5 bar (abs)
Oil ISO VG 10 density(ρ_l)	830 kg/m³
viscosity (μ_l)	10.6 cP at 34 °C
Air density (ρ_{ga})	1.2 kg/m³ at 1bar
viscosity(μ_{ga})	0.02 cP at 20 °C, 1 bar (abs)
Shaft speed (Ω_{max})	3.5 krpm
surface speed $\frac{1}{2} D\Omega_{max}$	23 m/s
Sparger pore size	2 μm
Air bubble size	Up to 4 mm

Five test seals

D/c~ 640

Smooth surface plain seal

Nominal c and worn ($>c$)

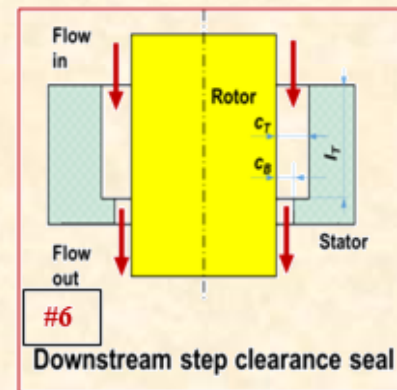
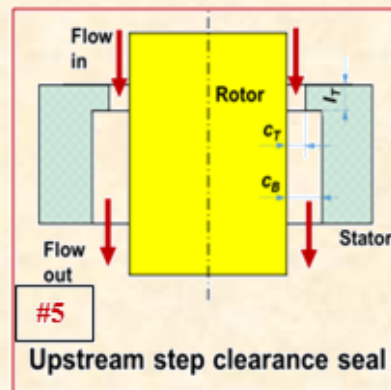
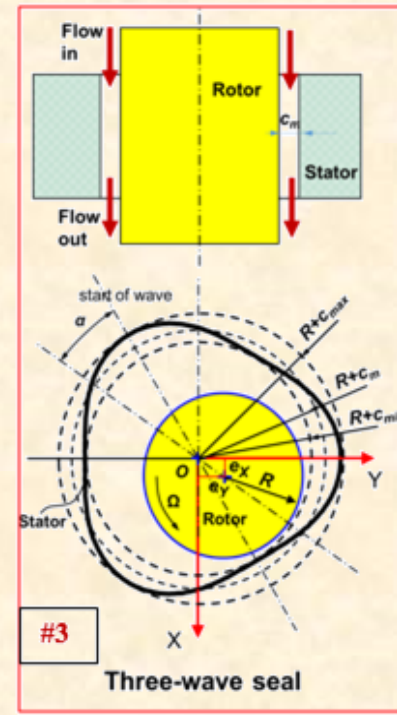
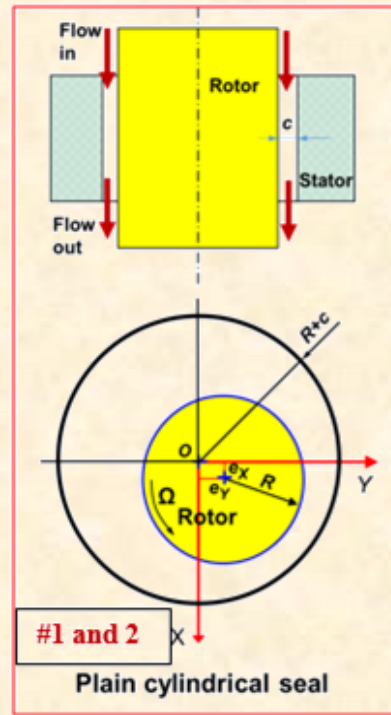
Three-wave seal:

Large dynamic stiffness

(Rim) step

clearance seals:

Used in hydraulic turbines/pumps.



Plain seals #1 & 2:

$c_r = 0.203$ mm,

$c_b = 0.274$ mm

(worn clearance)

#3

Three-wave seal

($c_m = 0.191$ mm)

#4

Upstream step clearance

($c_r = 0.164$ mm, $c_b = 0.274$ mm,

$L_T = 0.11L$).

#5

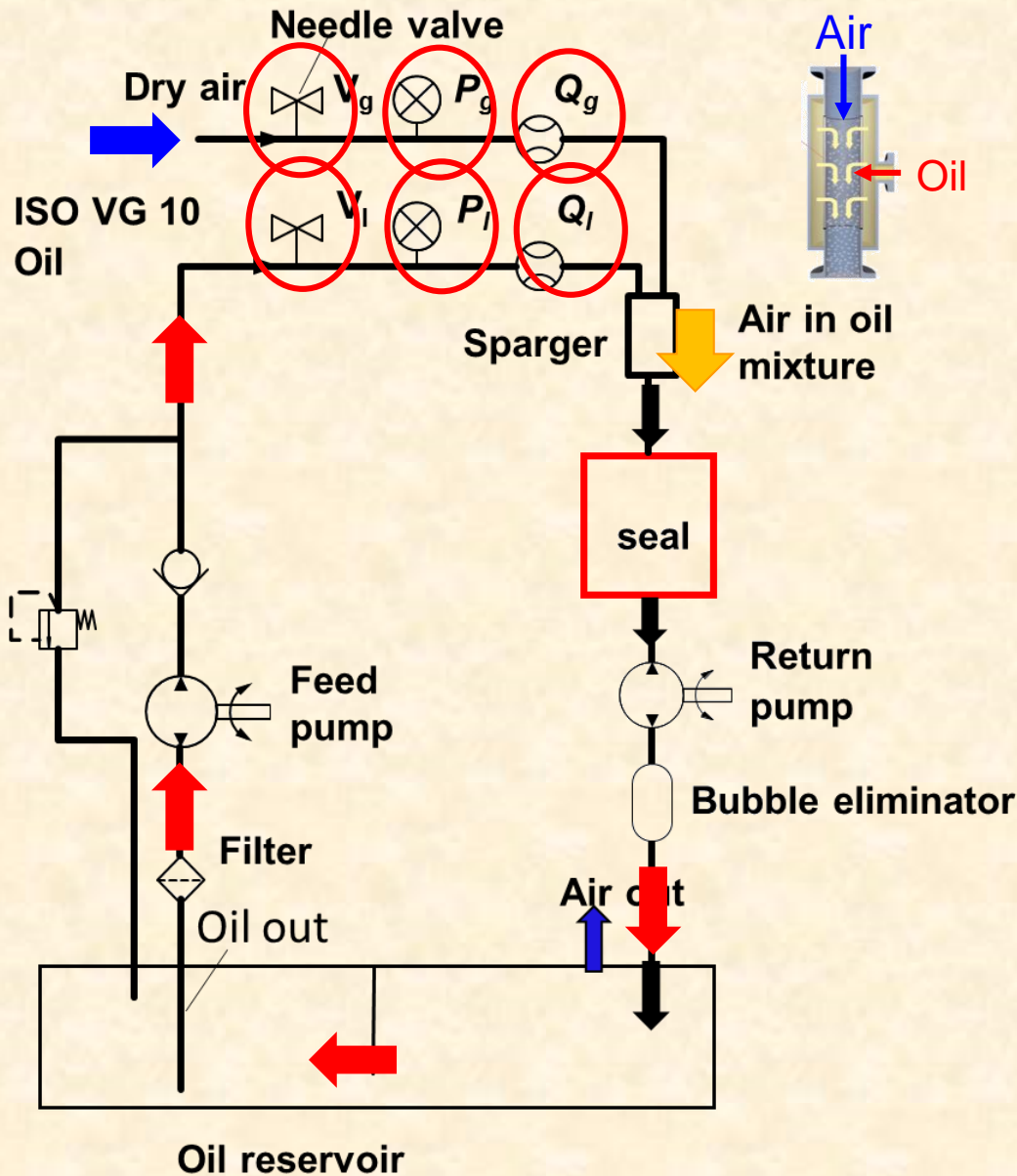
Downstream step

clearance

($c_r = 0.274$ mm, $c_b = 0.164$ mm,

$L_T = 0.82L$).

Air and oil circulation systems



α : Gas volume fraction

P_s : pressure at seal inlet plane

P_a : ambient pressure= 1 bar(a)

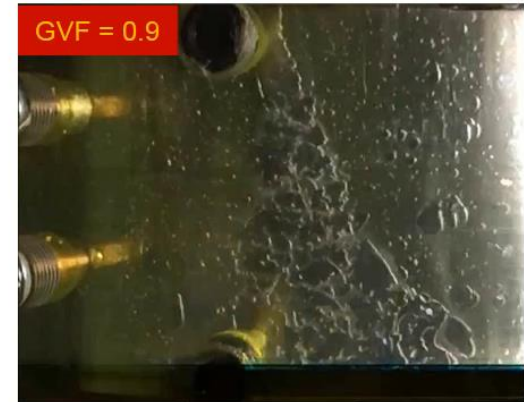
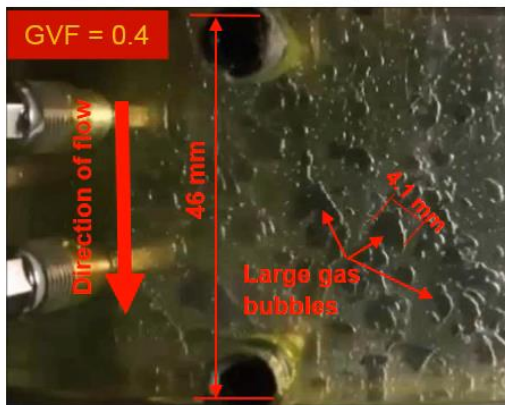
Q_g : gas flow rate at P_s

Q_l : liquid flow rate

GVF at inlet:

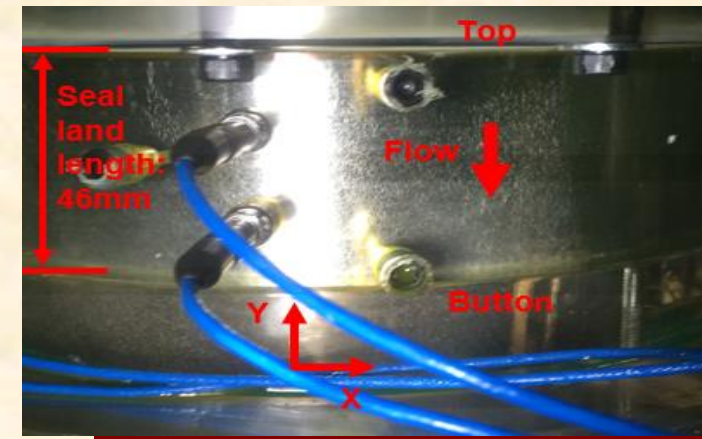
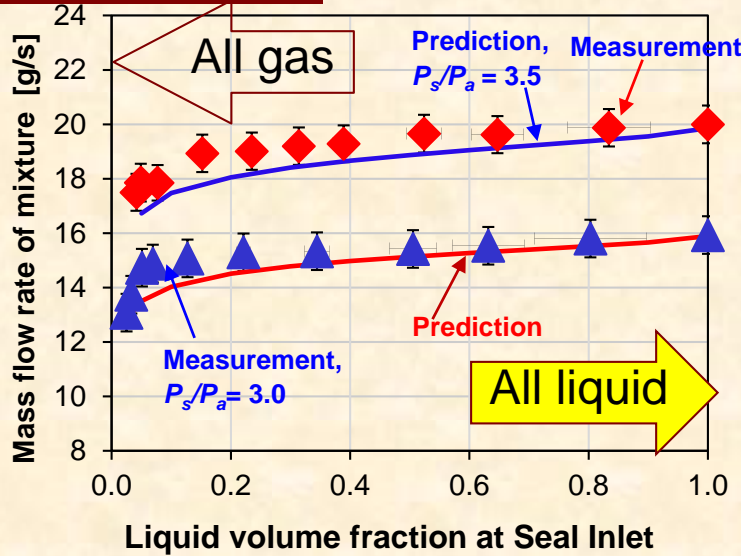
$$\alpha_{in} = \frac{Q_g \left(P_a / P_s \right)}{Q_l + Q_g \left(P_a / P_s \right)}$$

Flow visualization → inlet GVF = 0-0.9. $P_s/P_a=2.5$. Speed 0 rpm



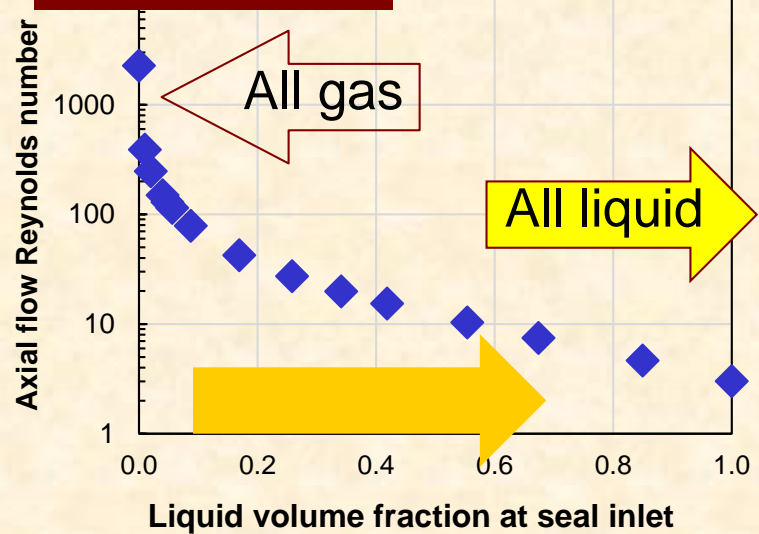
Plain seal : flow rate vs LVF (0 rpm)

Leakage



- Leakage increases with inlet LVF.
- Reynolds # drops from $> 1,000$ (air) to low magnitude as LVF increases.

Reynolds

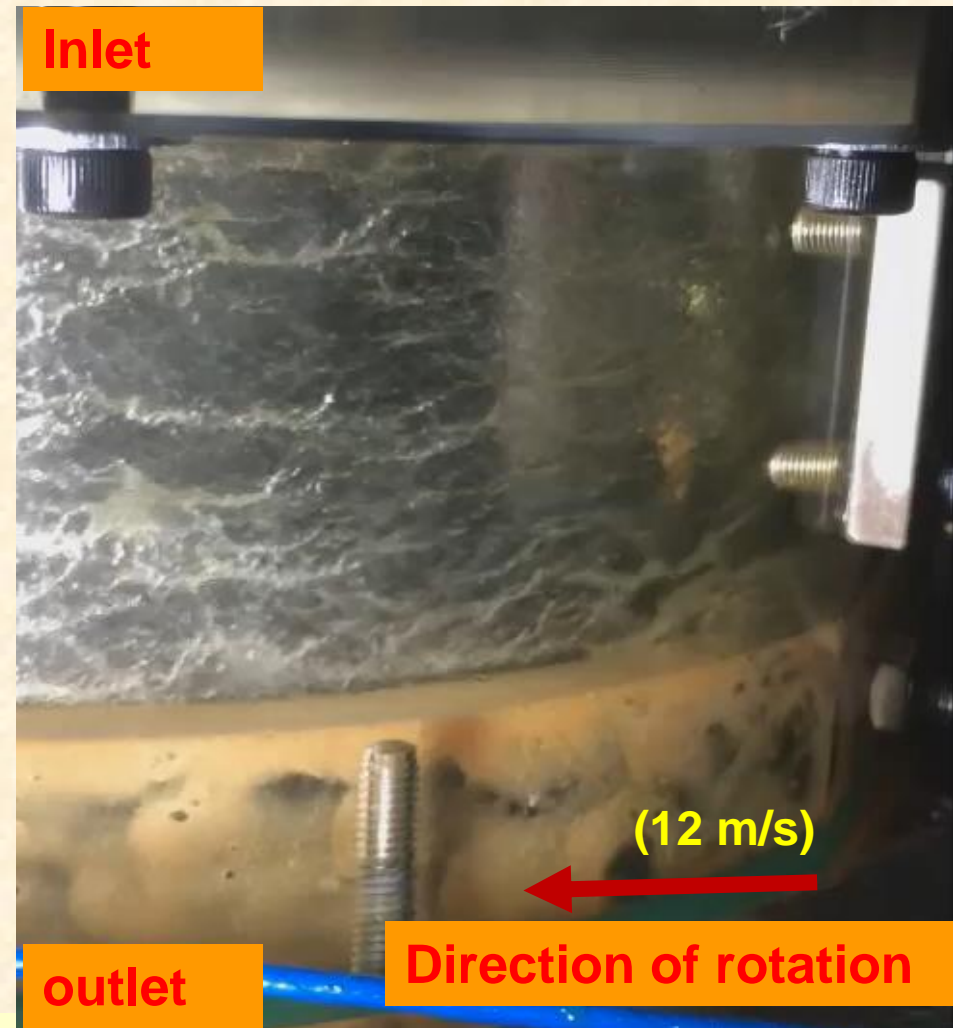


Flow with shaft spinning

$P_s/P_a = 2$, speed 1.8 krpm

Stroboscope light
with frequency 30
Hz freezes shaft
motion

Air bubbles
coalesce and
merge to make
streamlets →



Laminar flow Reynolds #:
 $Re_c = 153$, $Re_z = 245$ at exit plane

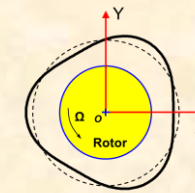
Seals' leakage and drag torque



Leakage (oil only)

LVF=1 (liquid only)

Normalized to:
$$m_l = \frac{1}{12} \frac{\rho_l}{\mu_l} \pi D c^3 \frac{\Delta P}{L}$$



Plain seals #1 & 2:
($c_1 = 0.203$ mm, $c_2 = 0.274$ mm)

#3
Three-wave seal
($c_m = 0.191$ mm)

#4
Grooved seal
($c_f = 0.211$ mm)

Upstream step clearance
($c_T = 0.164$ mm, $c_B = 0.274$ mm,
 $L_T = 0.11L$).

Downstream step clearance
($c_T = 0.274$ mm, $c_B = 0.164$ mm,
 $L_T = 0.82L$).

Three-wave seal leaks more than plain seal.

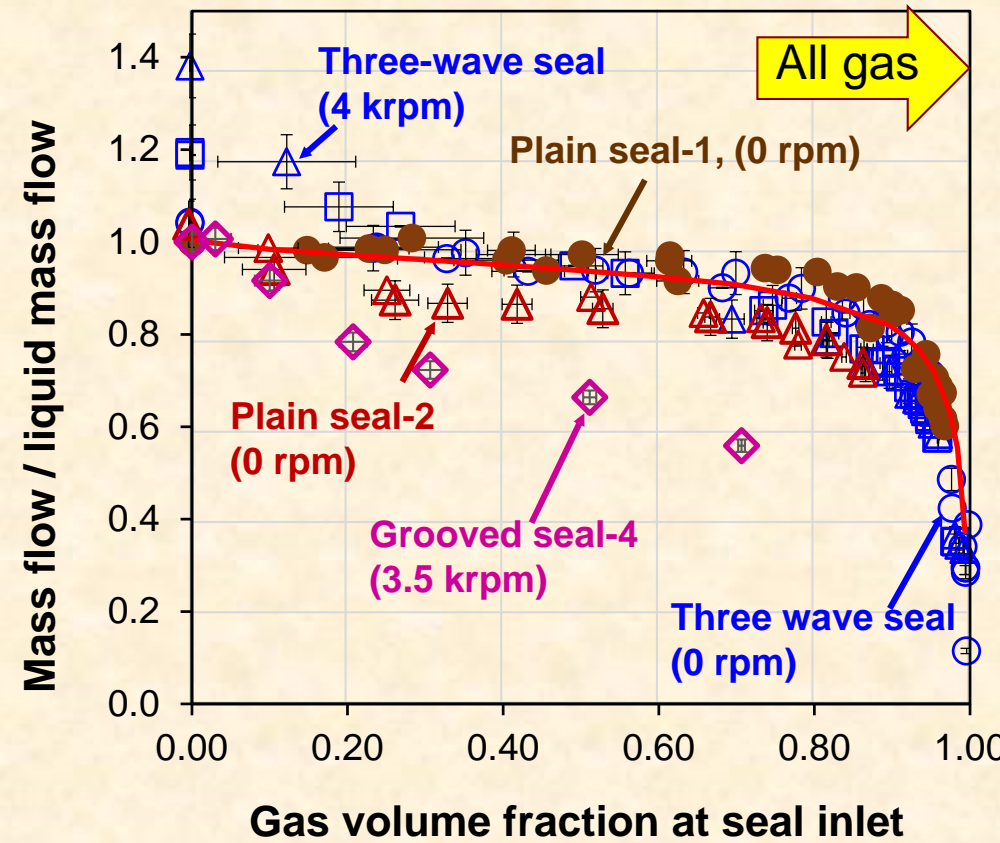
Leakage (Mixture) → gas volume fraction increases

Normalized with respect to liquid (GFV=0)

$$m = \frac{m_{mixture}}{m_{liquid}}$$

Leakage for all seals shows same trend as GVF increases → it drops!

Predictions agree with test data.



$C_{seal\#1} = 0.203$ mm; $C_{seal\#2} = 0.274$ mm
 $C_{seal\#3} = 0.191$ mm; $C_{seal\#4} = 0.211$ mm

Drag torque (mixture) T_{seal}

Shaft speed:
1.5, 2.5, 3.5 krpm

normalized to all liquid condition

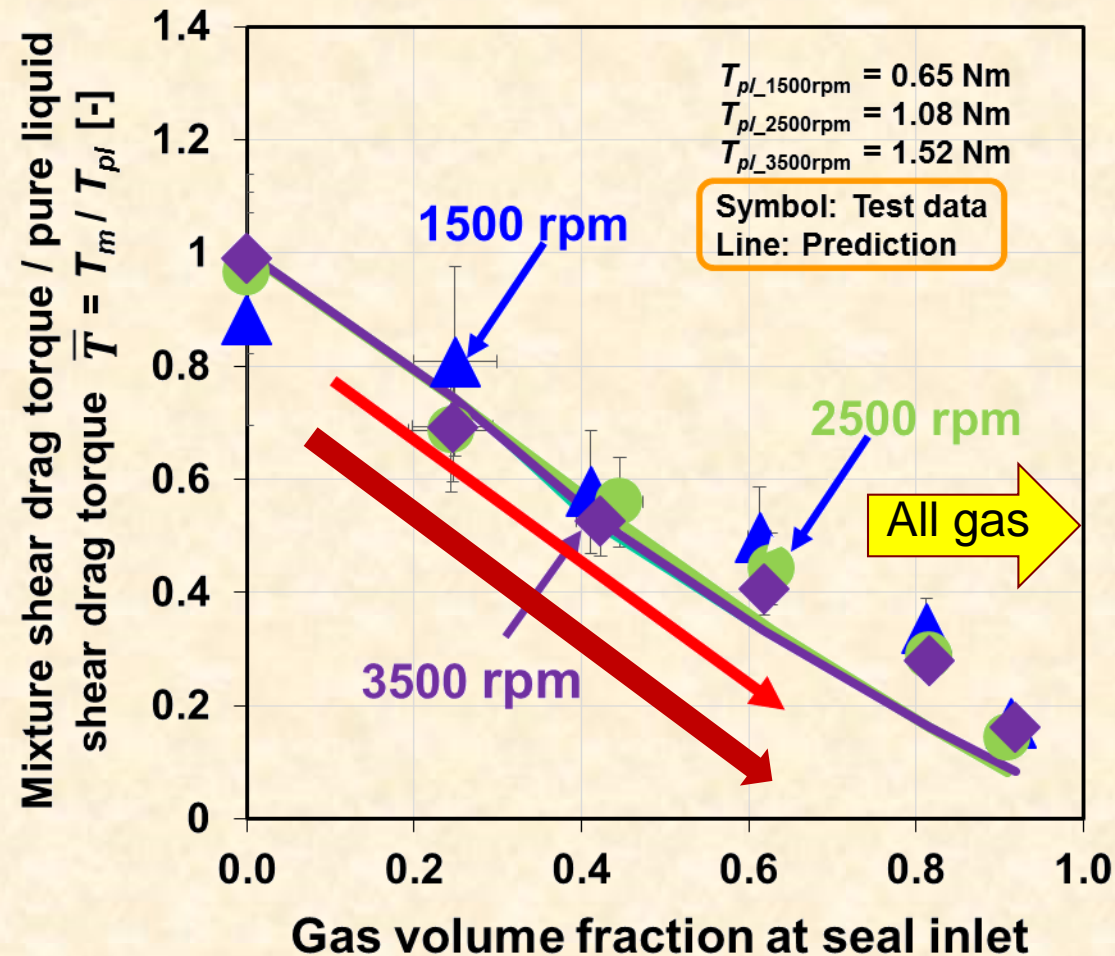
prediction

$$T_{seal} \sim \frac{2\pi \mu_{(GVF)} \Omega R^3 L}{c}$$

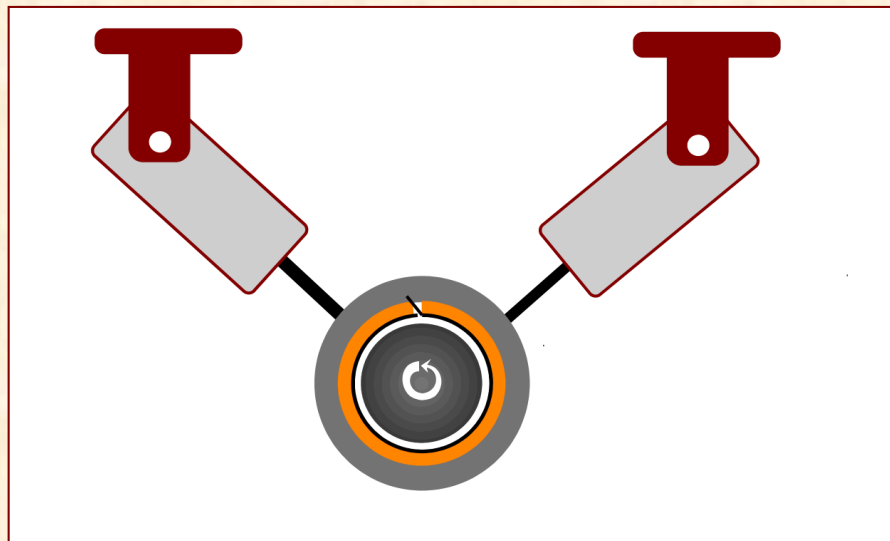
Torque linearly
decreases with GVF.

$GVF = 0 \rightarrow 0.9$
85% reduction in
torque

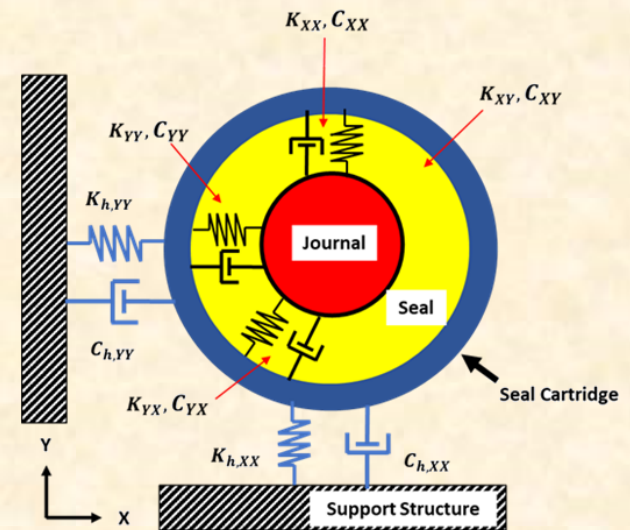
Grave implication for
pump and motor
reliable performance.



Experimental identification of force coefficients

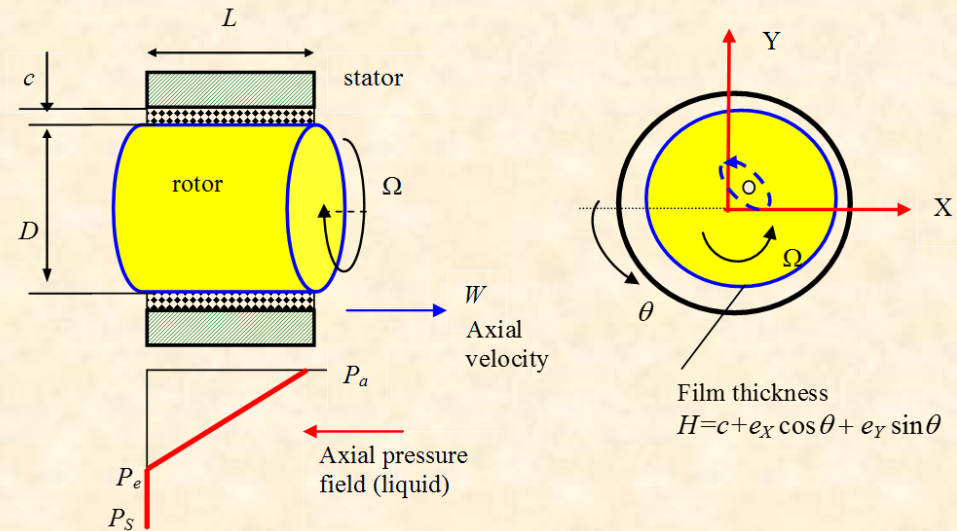


2-DOF system for seal and support structure



Dynamic force coefficients

For small amplitudes of rotor motion, a seal force is represented with **stiffness** (K), **damping** (C) and **inertia** (M) force coefficients:



$$\begin{Bmatrix} F_X \\ F_Y \end{Bmatrix} = - \begin{bmatrix} K & k \\ -k & K \end{bmatrix} \begin{Bmatrix} x \\ y \end{Bmatrix} - \begin{bmatrix} C & c \\ -c & C \end{bmatrix} \begin{Bmatrix} \dot{x} \\ \dot{y} \end{Bmatrix} - \begin{bmatrix} M & 0 \\ 0 & M \end{bmatrix} \begin{Bmatrix} \ddot{x} \\ \ddot{y} \end{Bmatrix}$$

$$\begin{Bmatrix} F_X \\ F_Y \end{Bmatrix} = - \begin{bmatrix} K_{(\omega)} & k_{(\omega)} \\ -k_{(\omega)} & K_{(\omega)} \end{bmatrix} \begin{Bmatrix} x \\ y \end{Bmatrix} - \begin{bmatrix} C_{(\omega)} & c_{(\omega)} \\ -c_{(\omega)} & C_{(\omega)} \end{bmatrix} \begin{Bmatrix} \dot{x} \\ \dot{y} \end{Bmatrix}$$

For two-phase flow or a gas

Identification of Force Coefficients

1) Apply Load $\mathbf{F} = \mathbf{F}_0 \sin(\omega t) \rightarrow$

Measure vectors of displacements $\mathbf{z} = \{x, y\}^T$, & accelerations $\mathbf{a} = \{a_x, a_y\}^T$

2) $\bar{\mathbf{F}}, \bar{\mathbf{A}}, \bar{\mathbf{Z}}$ = Discrete Fourier Transform of $\mathbf{F}, \mathbf{a}, \mathbf{z}$

$$3) \bar{\mathbf{F}} - \mathbf{M}_h \bar{\mathbf{A}} - [\mathbf{K}_h + i\omega \mathbf{C}_h] \bar{\mathbf{Z}} \rightarrow \mathbf{H}_{(\omega)} \bar{\mathbf{Z}}$$

$[\mathbf{M}, \mathbf{K}, \mathbf{C}]_h$ = mass, stiffness, damping of support structure

Components of seal complex stiffness H



$$\text{Re}(\mathbf{H}_{(\omega)}) \rightarrow \mathbf{K}_{(\omega)}$$

Dynamic Stiffness

$$\text{Im}(\mathbf{H}_{(\omega)}) \rightarrow \omega \mathbf{C}_{(\omega)}$$

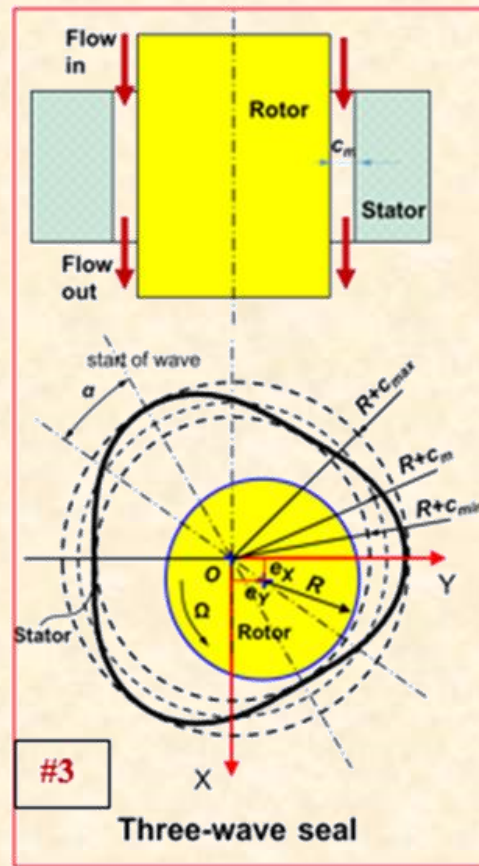
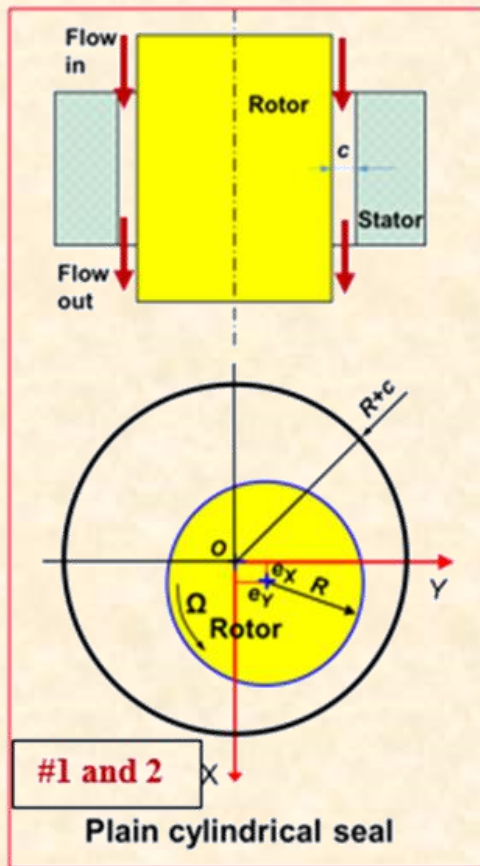
Proportional to Damping



$$C_{eff} = C - k/\omega = [\text{Im}(H_{xx}) - \text{Re}(H_{xy})]/\omega$$

Effective Damping

Force coefficients for plain cylindrical seals and three-wave seal



#1 & #2

Plain seals

$c_1=0.203$ mm, $c_2=0.274$ mm (worn)

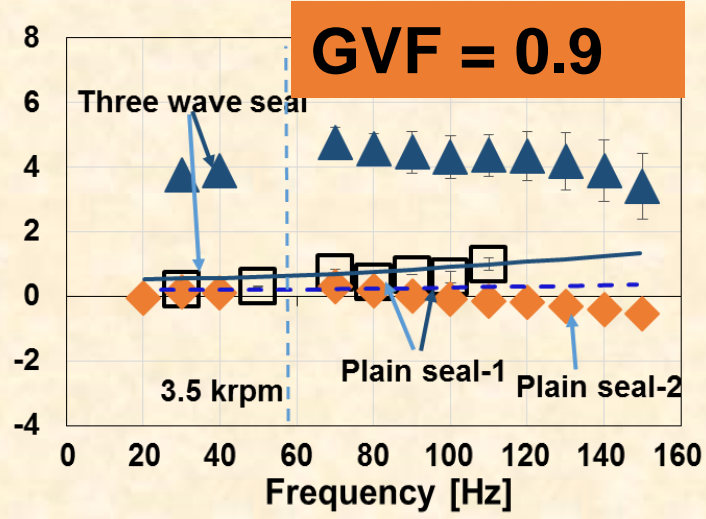
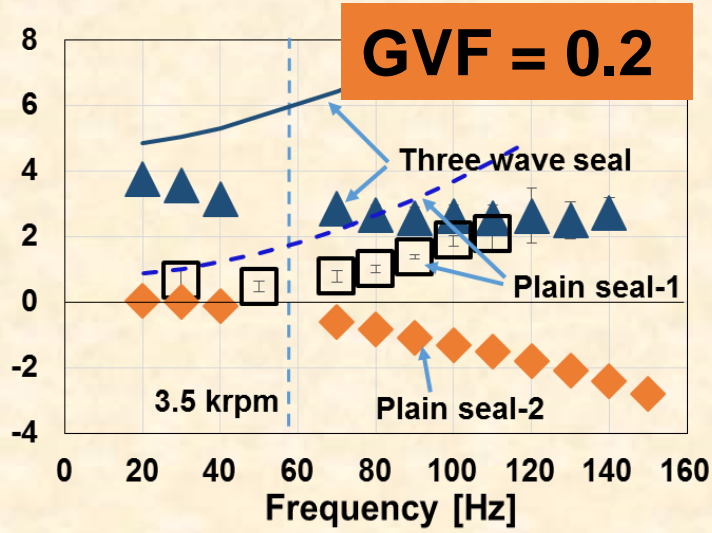
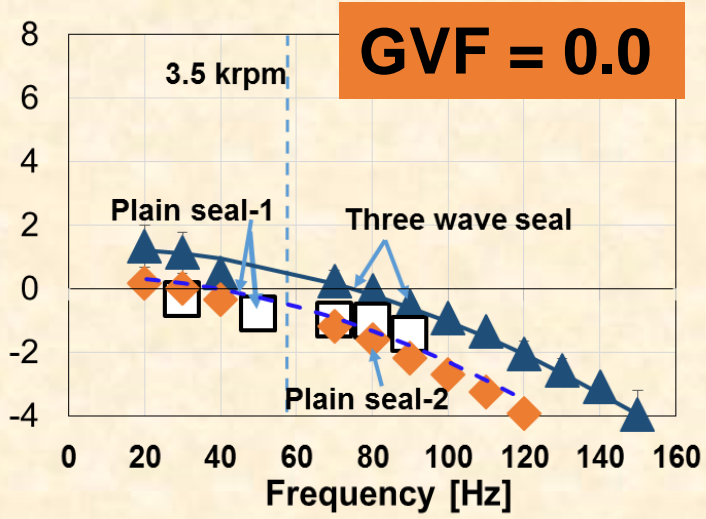
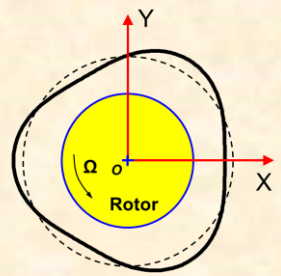
#3

Three-wave seal $c_m=0.191$ mm

Direct dynamic stiffness K (MN/m)

Symbols: test results Lines: predictions

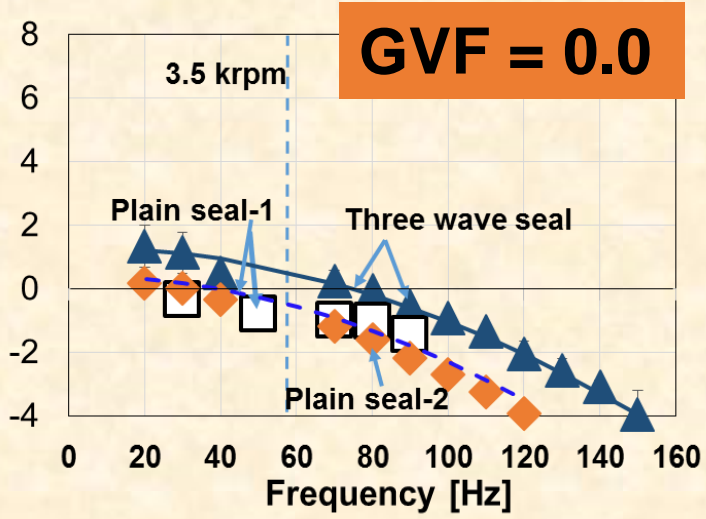
- Plain seal-1
- ◇ Plain seal-2
- ▲ Three-wave seal



Direct dynamic stiffness K (MN/m)

Symbols: test results Lines: predictions

- Plain seal-1
- ◇ Plain seal-2
- ▲ Three-wave seal

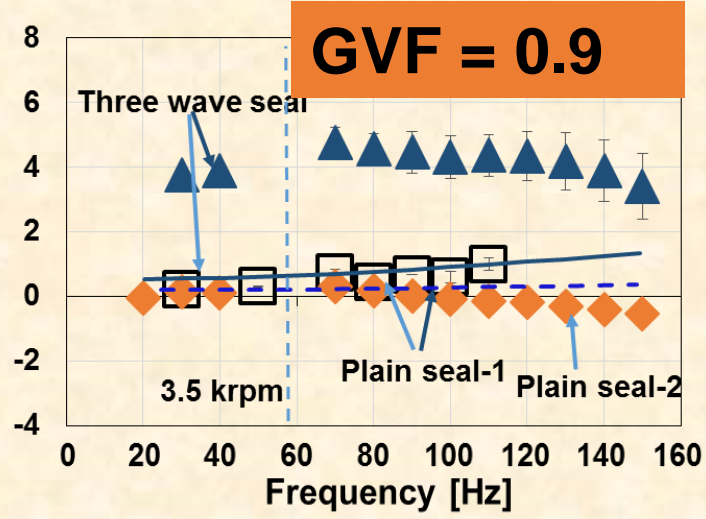


Three wave seal (#3) has largest K (promotes static stability).

Worn seal (#2) shows lowest K .

K : soft to hard as GVF increases.

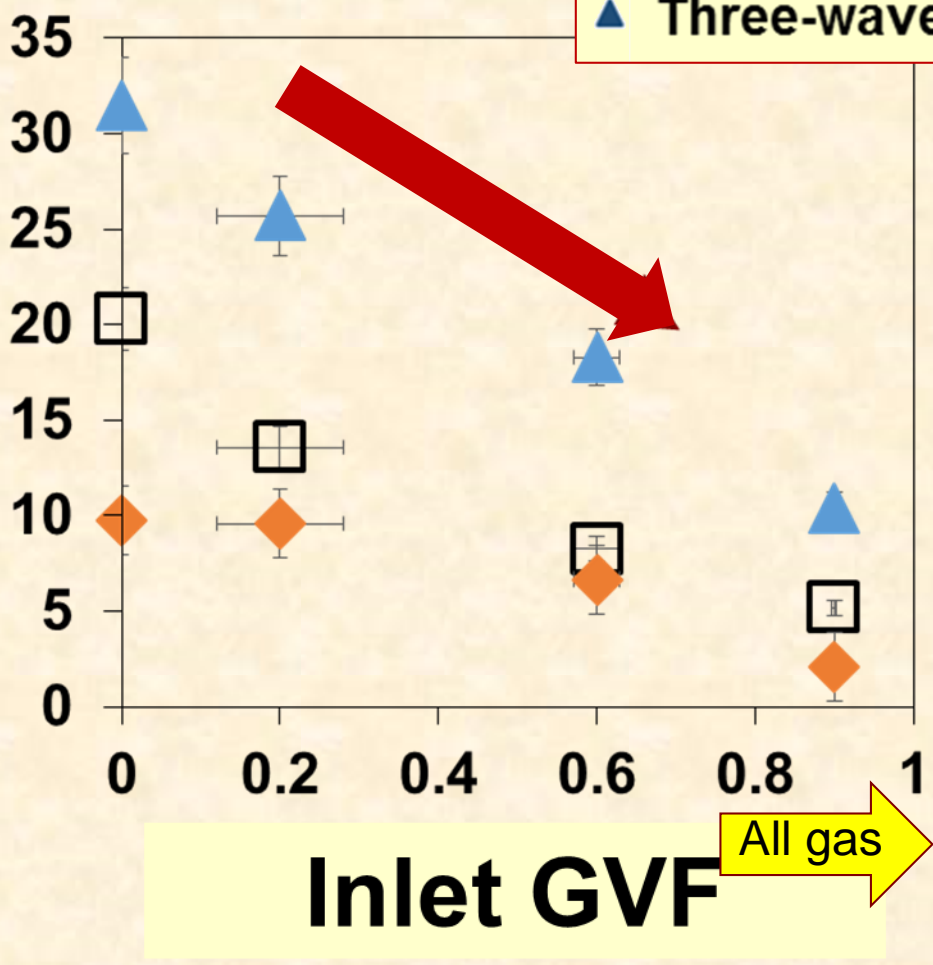
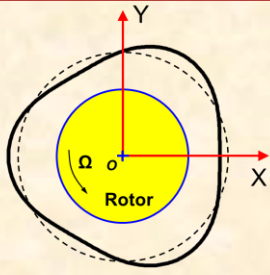
Lesser added mass!



Direct damping coefficient C (kN.s/m)

Symbols: test results

- Plain seal-1
- ◇ Plain seal-2
- ▲ Three-wave seal



C is frequency independent

Three wave seal (#3) has largest C .

Worn seal (#2) shows smallest C .

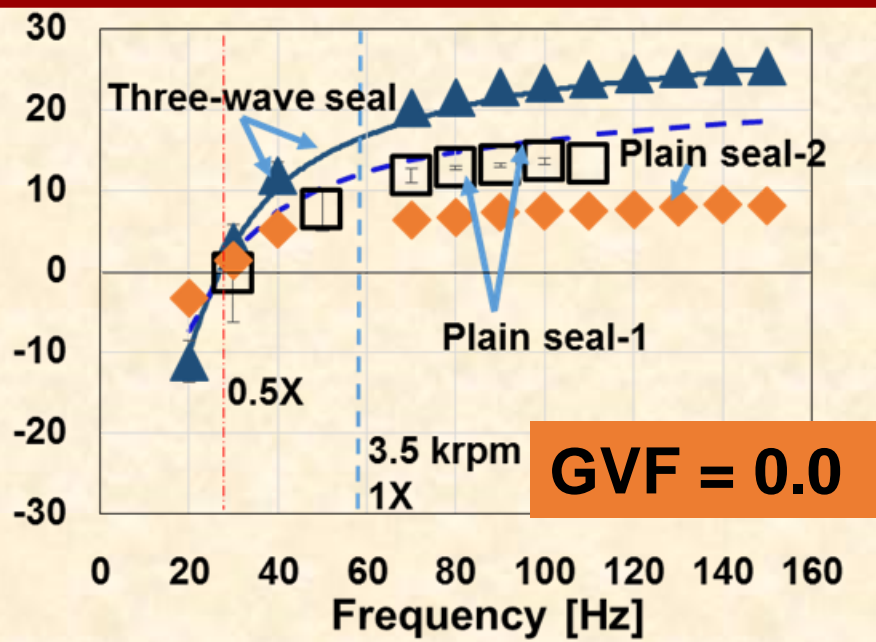
C drops with GVF

$C \sim C_1(1-GVF)$

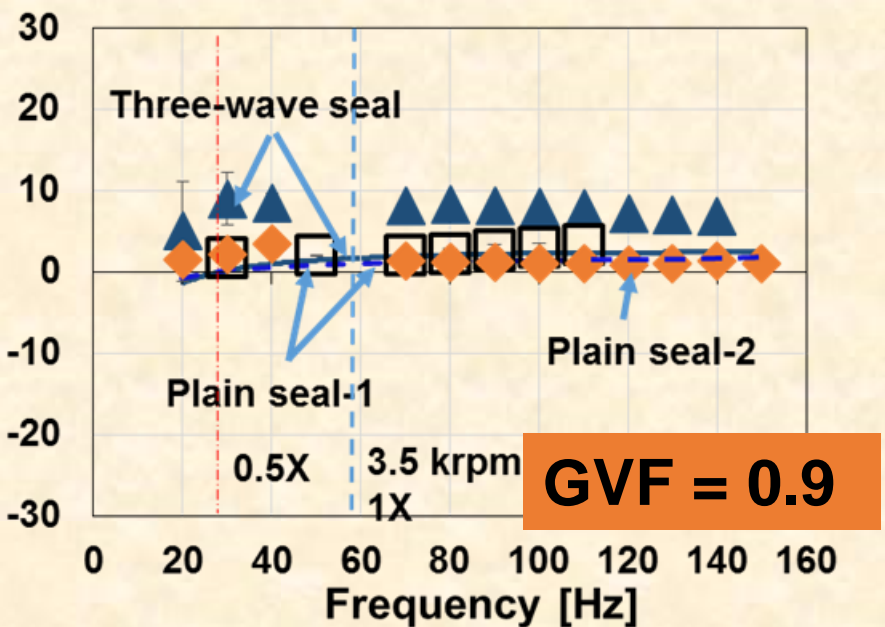
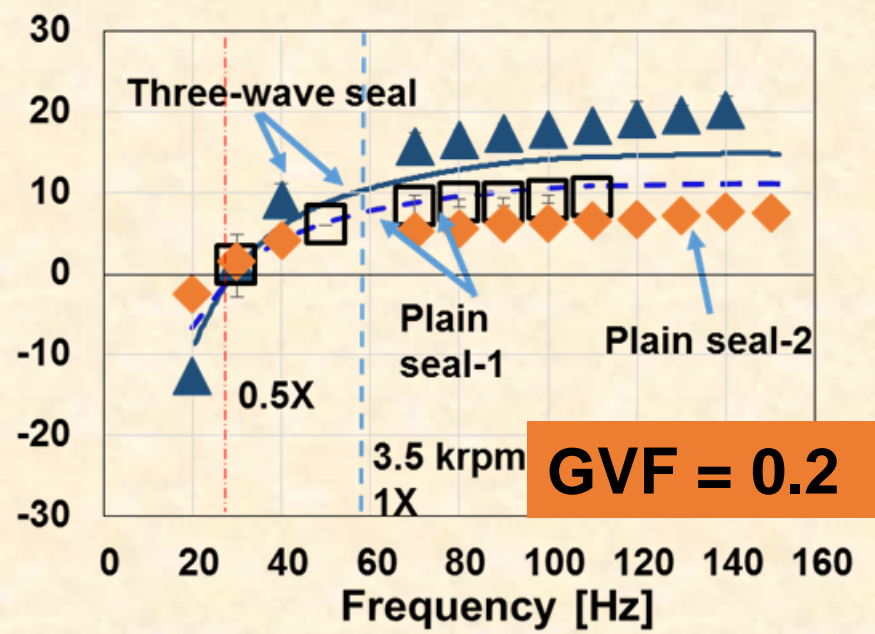
Effective damping (kN.s/m)

$$C_{eff} = C - k/\omega$$

Symbols: test results Lines: predictions



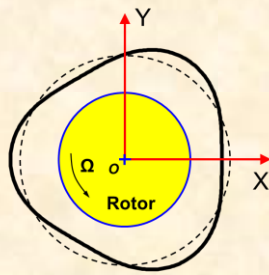
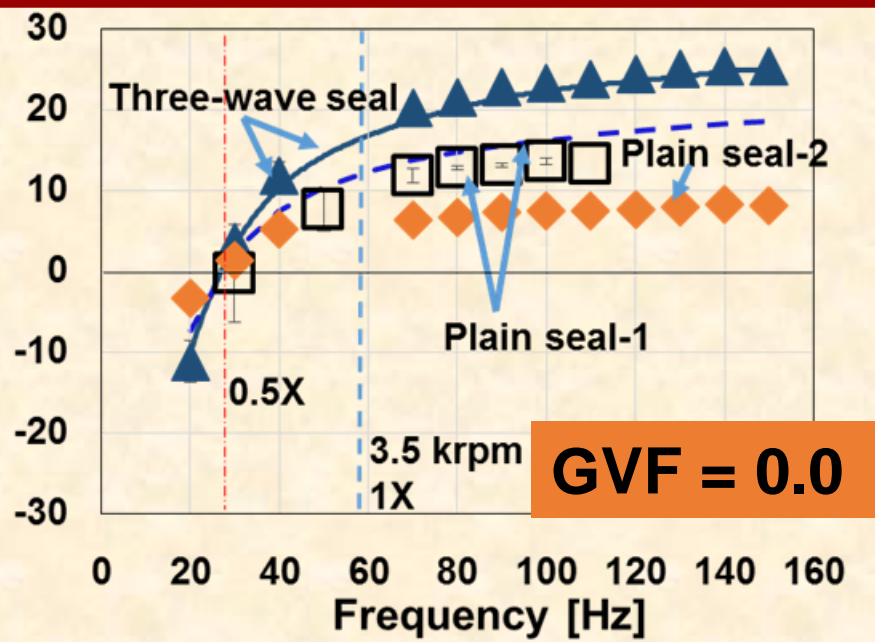
- Plain seal-1
- ◇ Plain seal-2
- ▲ Three-wave seal



Effective damping (kN.s/m)

$$C_{eff} = C - k/\omega$$

Symbols: test results Lines: predictions

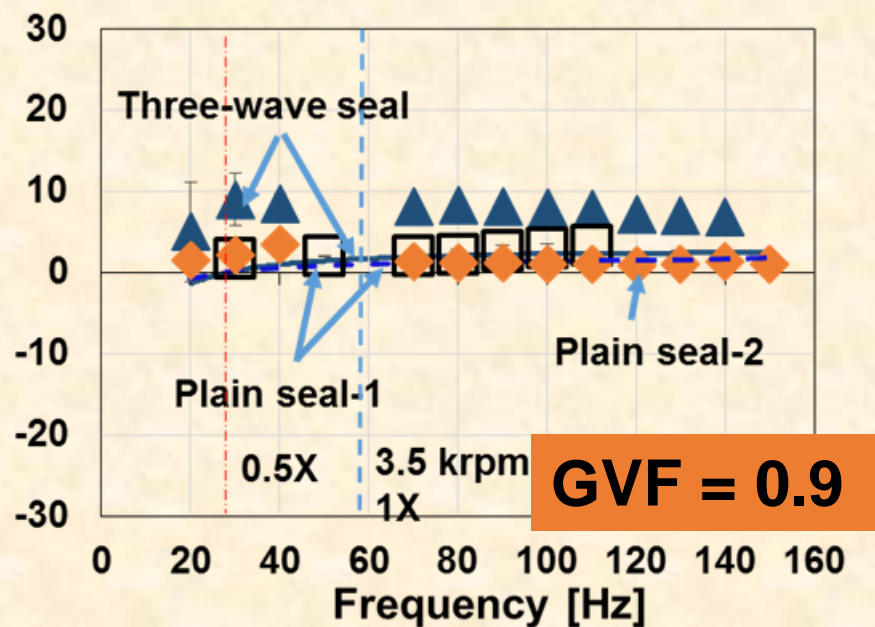


- Plain seal-1
- ◆ Plain seal-2
- ▲ Three-wave seal

For stability, $C_{eff} > 0$ is a must.

Increase in GVF $\rightarrow C_{eff}$ drops.

Cross frequency drops from $\sim \frac{1}{2} X$ to a low magnitude.

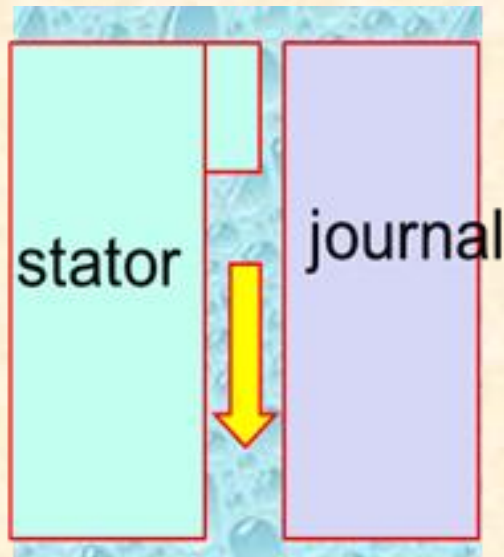


Force coefficients for step clearance seals

Typical rim seals in hydraulic turbines

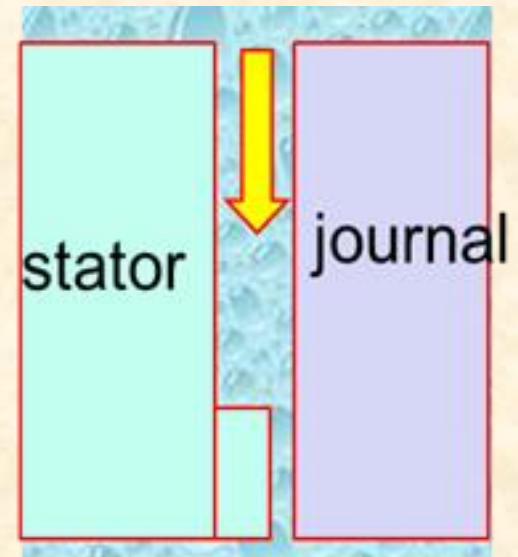
Upstream step clearance

$c_T=0.164$ mm, $c_B=0.274$ mm, $L_T=0.11L$



Downstream step clearance

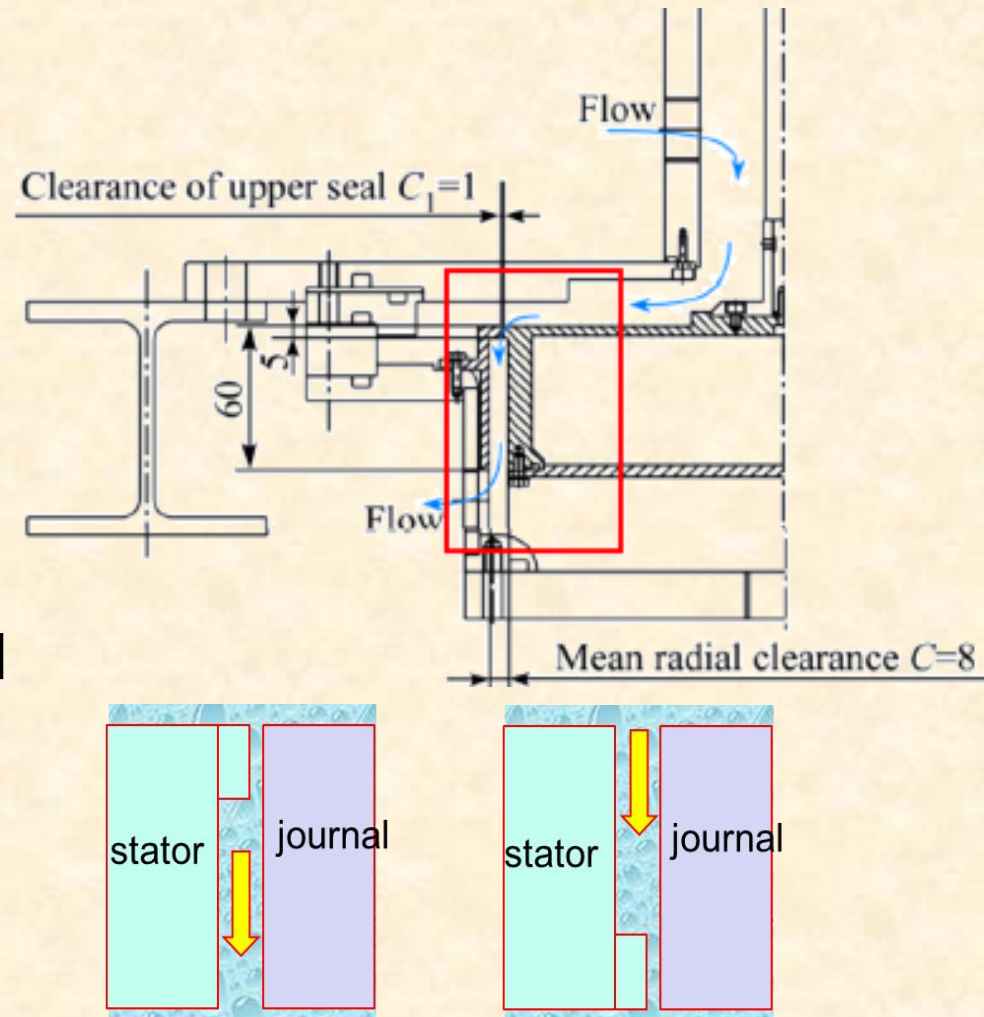
$c_T=0.274$ mm, $c_B=0.164$ mm, $L_T=0.82L$



Direction of flow

Step clearance seals in hydraulic turbines

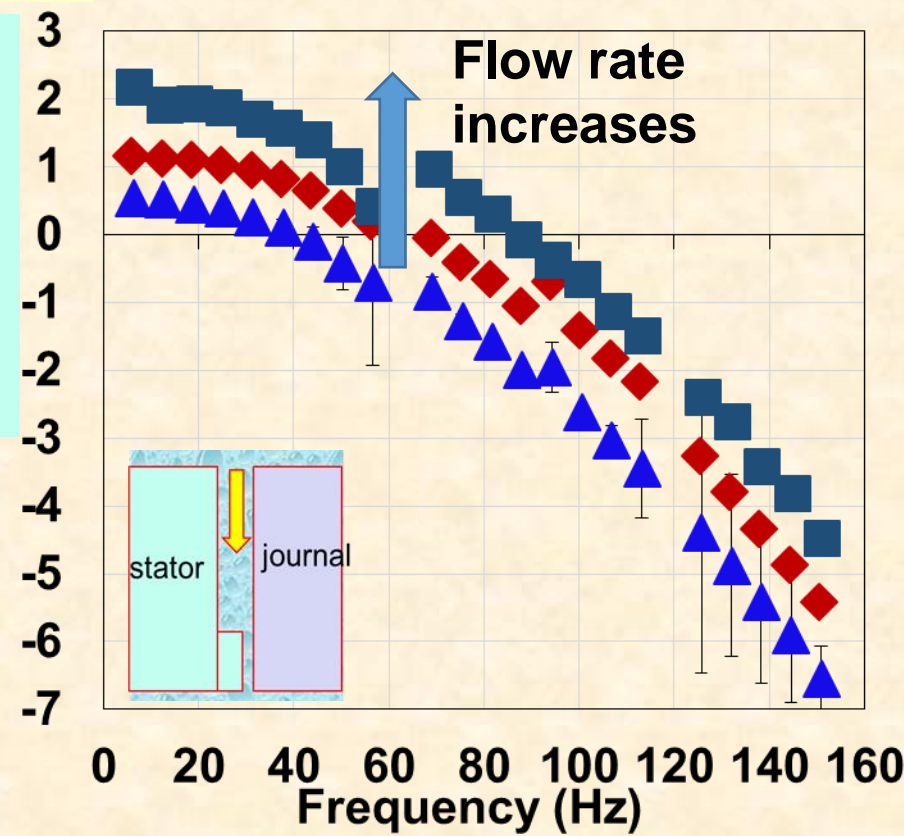
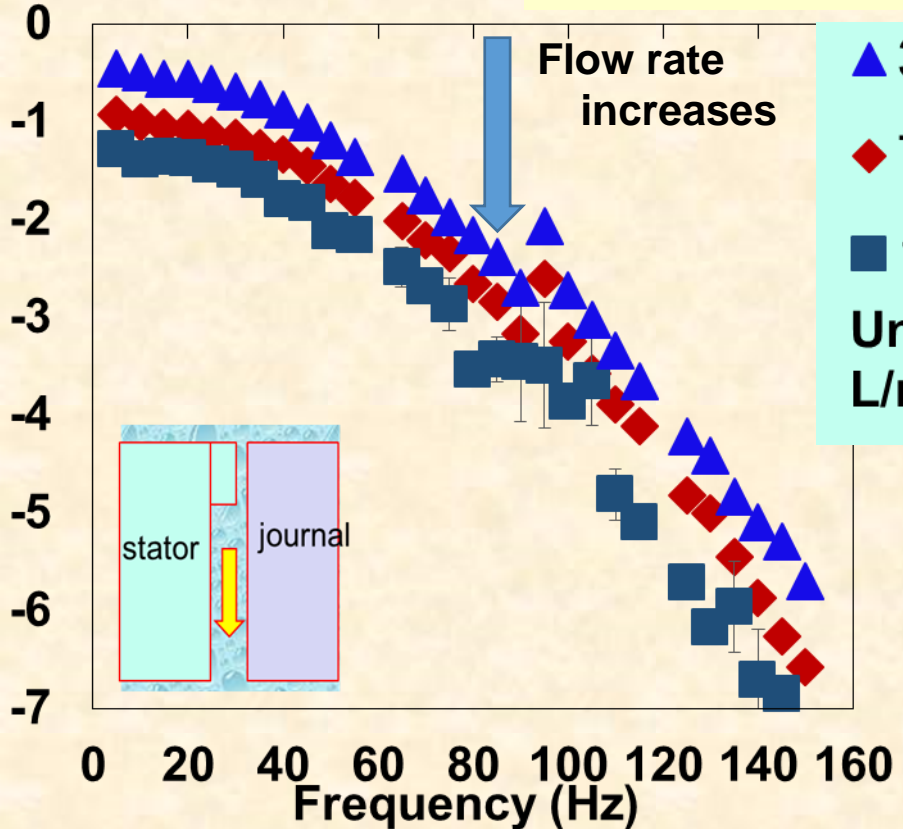
- Pump-turbines installed with (rim) upstream step clearance seals vibrate at a natural frequency (below structural one) & even w/o shaft rotation.
- But these units do not (self) vibrate when installed with a downstream step clearance seal.



Dynamic stiffness for **step clearance seals**

$Re(H) = K - \omega^2 M$ (MN/m)

0 rpm. Liquid only



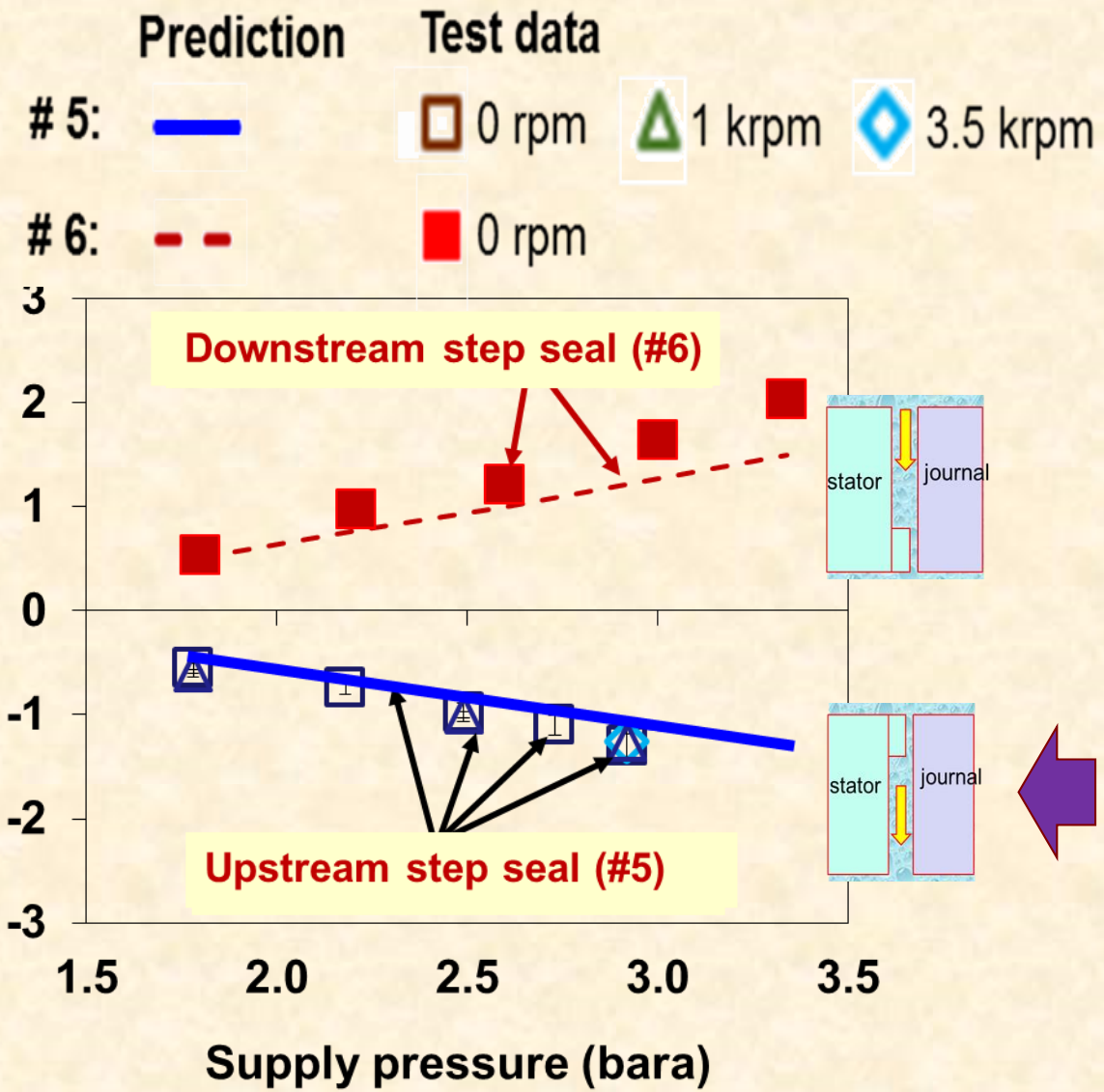
$K < 0, C > 0$

$K > 0, C > 0$

$|K|$ grows with flow rate (supply pressure)

Direct stiffness for **step clearance** seals $K_{(MN/m)}$

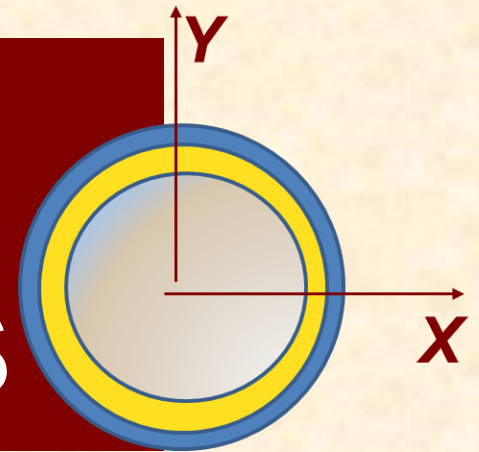
0 -3.5 krpm. Liquid only



$|K| \sim$ supply pressure (flow), not a function of shaft speed.

→ negative stiffness for upstream narrow clearance step seal may cause a static instability.

Air injection to increase stiffness



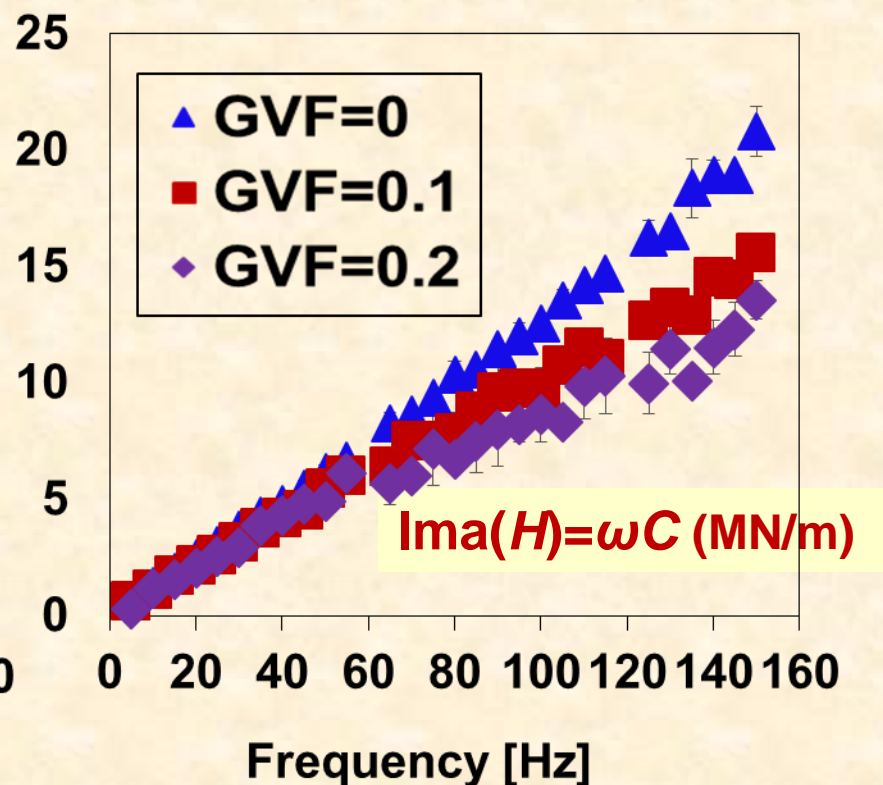
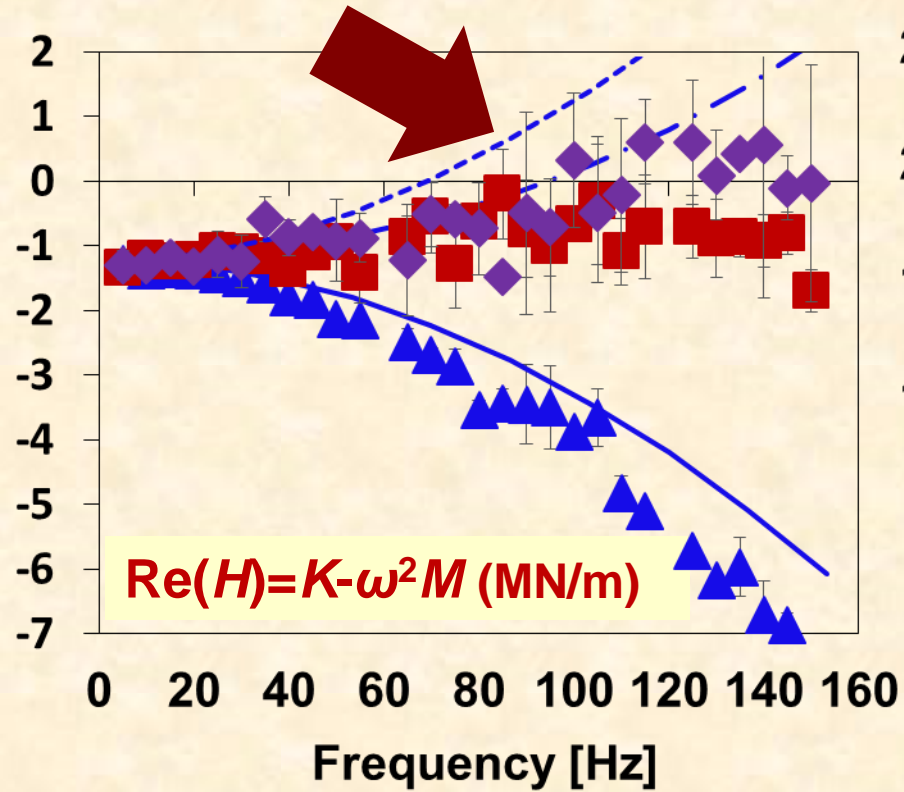
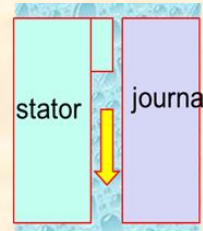
K

Air injection increases K (upstream step seal)!

- All liquid seal, $K < 0$ and reduces quickly with frequency.
- Air injection reduces damping but increases dynamic stiffness $\rightarrow K > 0$.

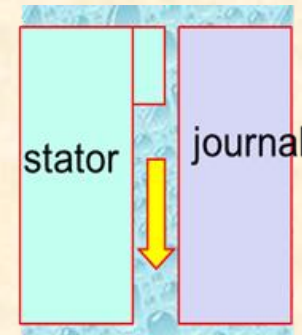
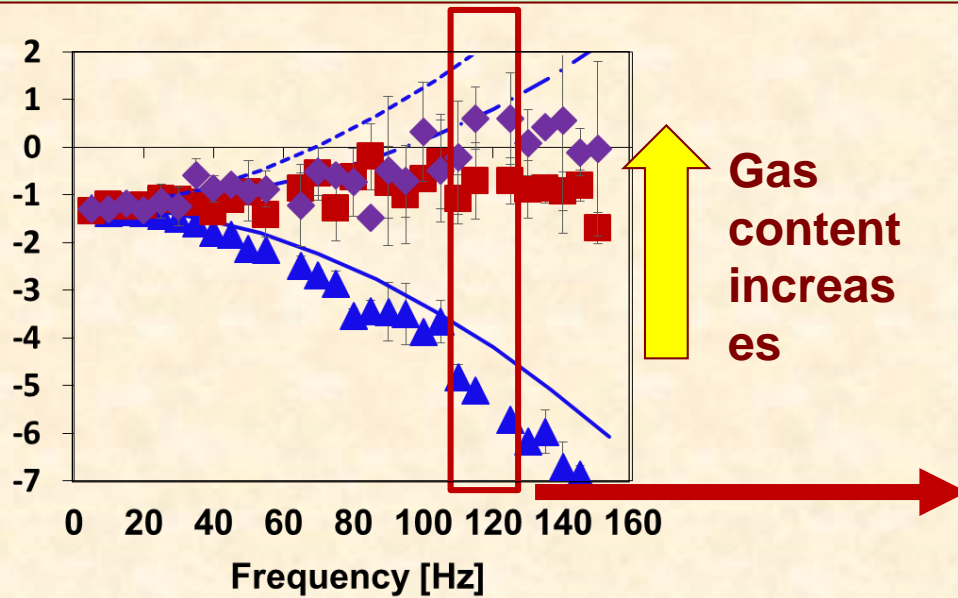
Symbols: test results

$Q_l = 11.4$ L/min, 0 rpm
 $P_s = 2.9$ bara



(upstream step seal)

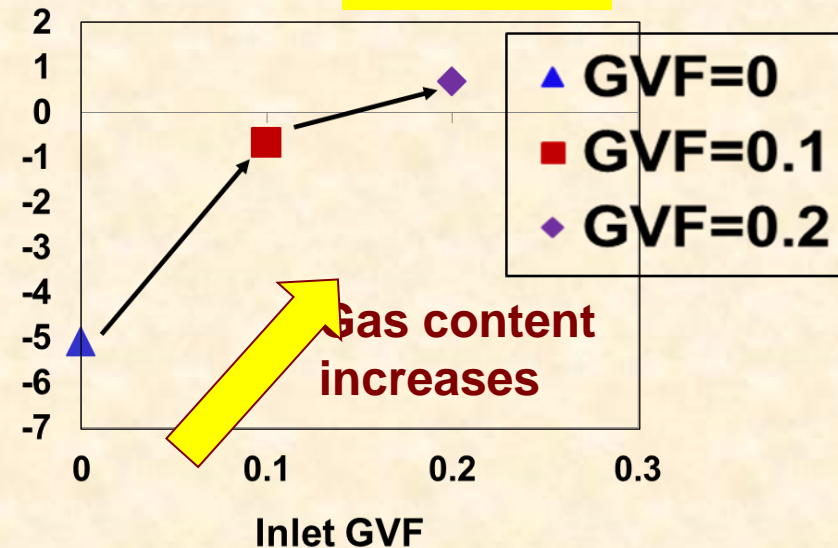
Air injection turns a negative stiffness into a positive centering one ($K > 0$).



0 rpm

$Q_i = 11.4$ L/min,
 $P_s = 2.9$ bara

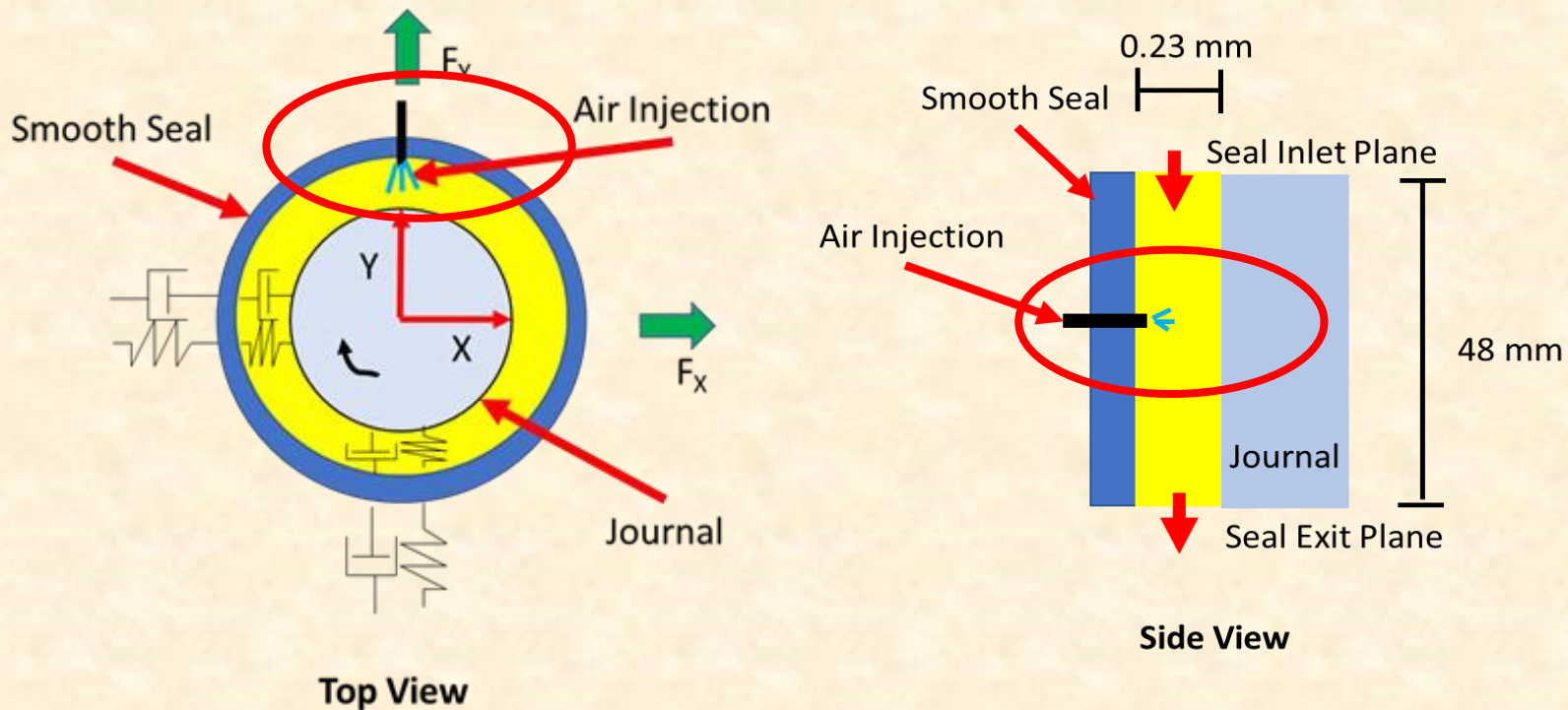
At 115 Hz



$K > 0$ brings static stability to vertical turbines.

Seal stiffness hardens due to quick drop in sound speed brought by the small amount of gas and exacerbated by excitation frequency.

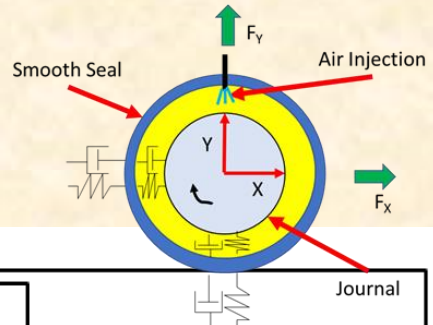
Bubbles injection to increase stiffness



Injection of bubbles reduces damping

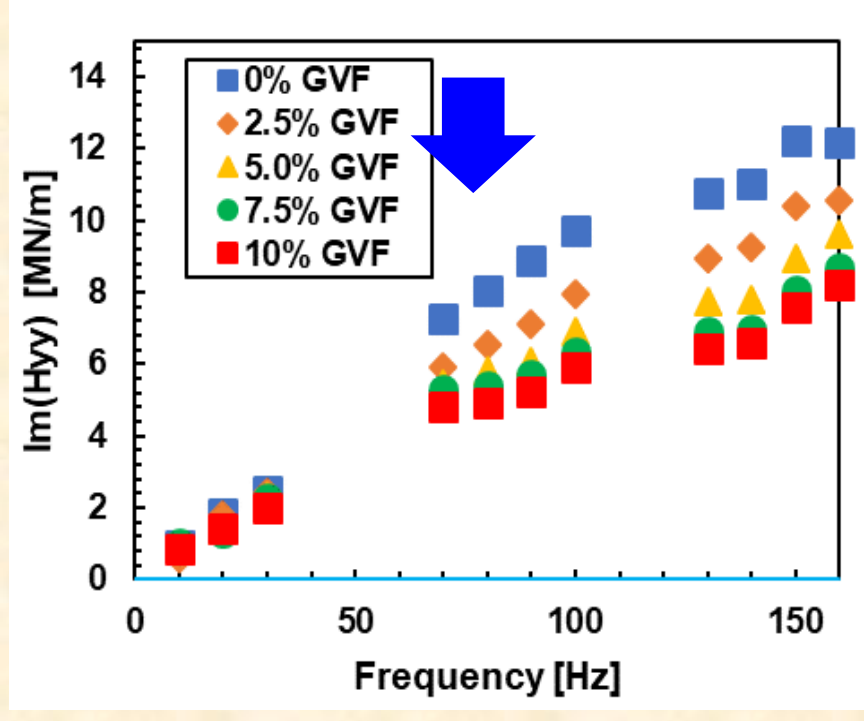
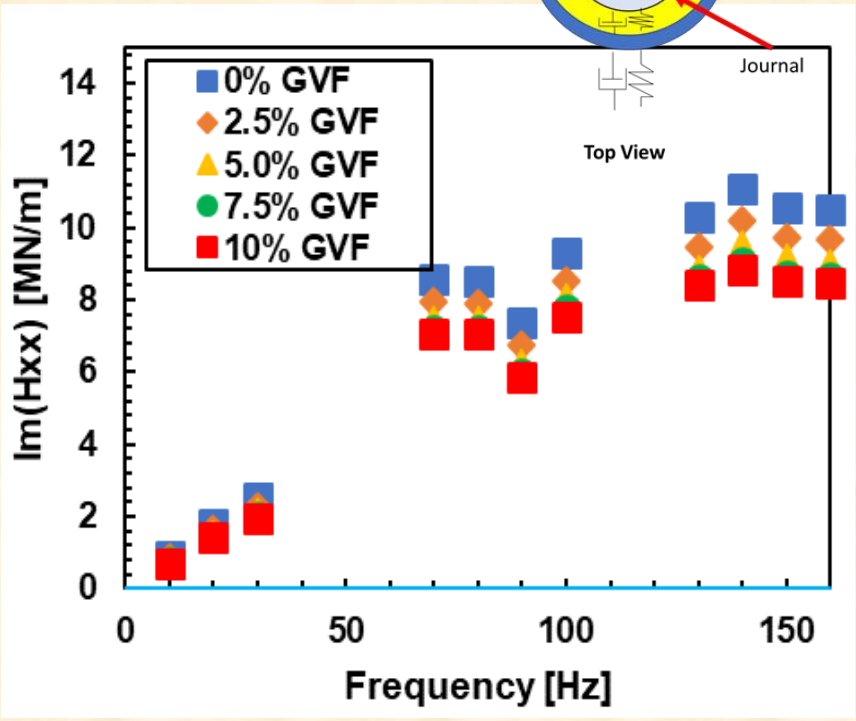
0 rpm,
Ps/Pa=2.5

$\sim C_{xx}$



$\sim C_{yy}$

Y- direction of bubbles injection

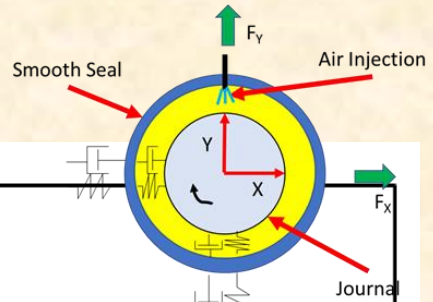


$C_{xx} > C_{yy} > 0$ as GVF increases

Injection of bubbles increases K

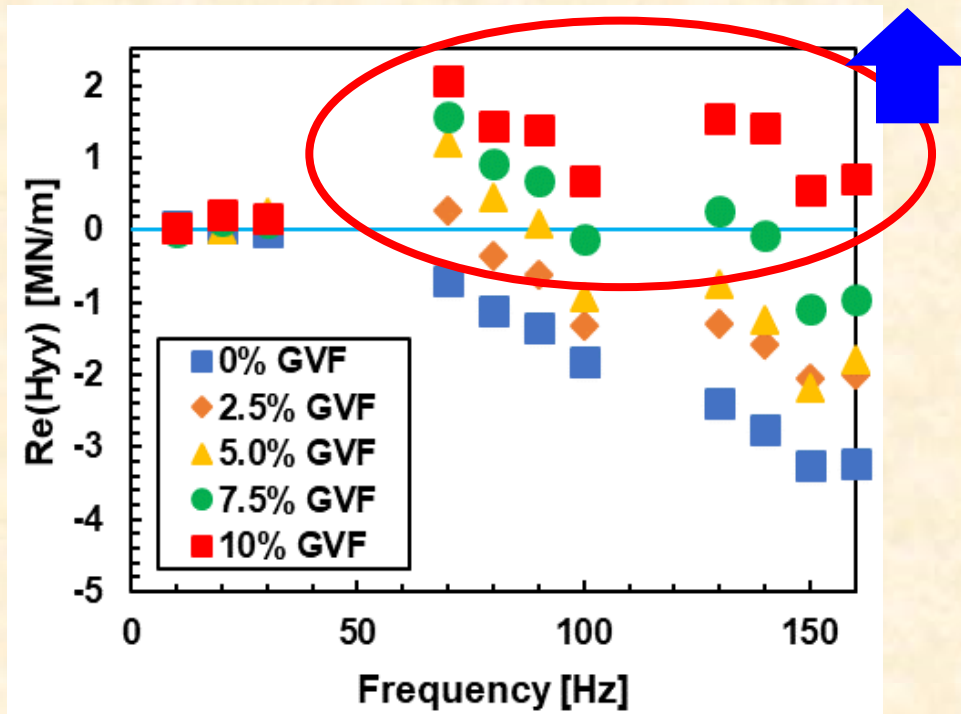
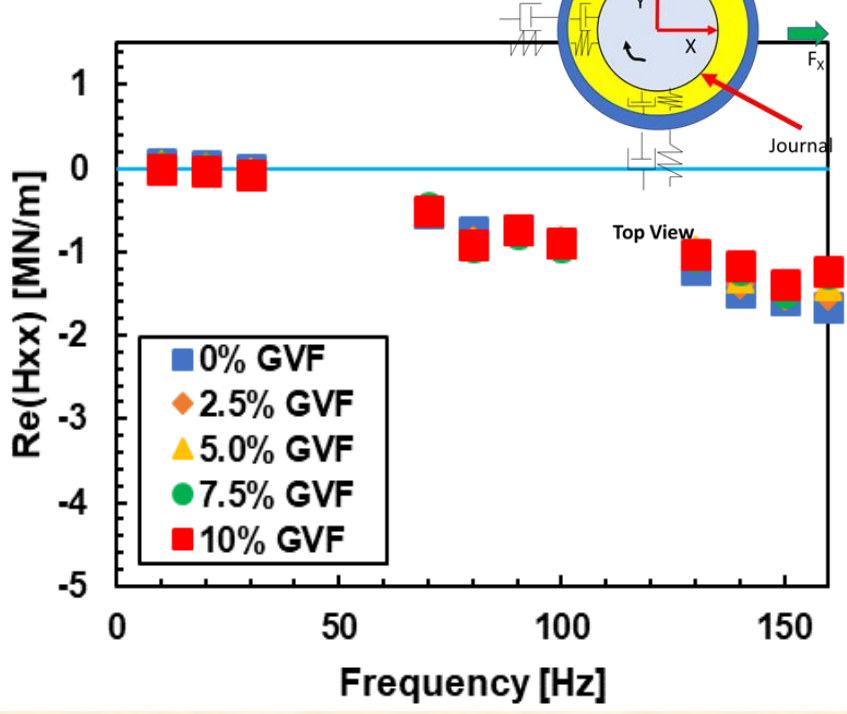
0 rpm,
 $P_s/P_a=2.5$

K_{xx}



K_{yy}

Y- direction of bubbles injection



$K_{xx} < 0, K_{yy} > 0$ as GVF increases

Stiffness asymmetry promotes rotor stability!

Conclusion

**ON PUMP SEALS OPERATING WITH
MULTIPLE PHASE CONDITIONS:
MEASUREMENTS AND GAS INJECTION TO
INCREASE SEAL CENTERING STIFFNESS**



Conclusion

- (a) Three wave seal leaks more than plain seal. The downstream step clearance seal leaks the least.
- (b) Mass flow rate and drag torque drop continuously with an increase in gas volume fraction (GVF).
- (c) Force coefficients are frequency dependent for operation with gas/oil mixtures.
- (d) Three wave seal shows largest direct stiffness K .
- (e) Cross stiffness k decreases with frequency and GVF.
- (f) Damping C decreases with GVF $\rightarrow C \sim C_1 (1 - \text{GVF})$
- (g) C_{eff} increases with frequency and drops with GVF. Cross over frequency is $\sim \frac{1}{2} X$.
- (h) Air injection produces seal stiffness hardening & asymmetry \rightarrow increases static stability (good for vertical systems).

Acknowledgments

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Learn more at

<http://rotorlab.tamu.edu>

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